

THE 34TH MULTIDISCIPLINARY ACADEMIC CONFERENCE

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BOOK OF OCEEDINGS

Bridging the Sub-Sahara Africa Development and Technology Frontiers: Integrating Sustainable Practice with Innovation TO Address African Challenges.

The 33rd Multidisciplinary Academic Conference Proceedings of Mediterranean Research and Publications International on Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara African Development and Technology Frontiers: An Innovation to Address African Challenges, Vol. 34 No. 2, 28th Sub-Sahara Af

PROCEEDING OF THE ACADEMIC CONFERENCE ON SUB-SAHARA AFRICAN DEVELOPMENT AND TECHNOLOGY FRONTIERS: AN INNOVATION TO ADDRESS AFRICAN CHALLENGES.

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RESPONSE SURFACE METHODOLGY (RSM) OPTIMIZATION AND CHARACHTERIZATION OF SILICA PRODUCTION FROM BIDA RICE HUSK

ADAMU M1., OLUTOYE, M. A2., ETERIGHO E. J2 AND YAHYA M. D2.

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Due to the fact that the compositions of silica derived from rice husk depends on the soil type and composition, type of fertilizer and chemicals used during planting and climate or geographical factors. In this particular research, the production of silica from rice husk obtained from Bida was optimized using Response Surface Methodology (RSM). The final silica produced at optimum conditions was characterized using XRF, XRD, SEM/EDX and BET. Preliminary investigations were conducted on the reaction variables which include: NaOH concentration, volume of NaOH, reaction temperature and reaction time. The results obtained were used to generate a design matrix using design expert 13.0 software via Box-Behnken Design (BBD). The software suggested a quadratic model that predicted the optimum yield of 7.655 g at optimum conditions of 3.0 M NaOH, 250 ml NaOH, 90 minutes reaction time and 100 °C reaction temperatures. The model fit statistics also shows that the predicted R2 value of 0.9141 is in agreement with the adjusted R2 value of 0.9654. The adequate precision of the model is 28.558 with an insignificant lack of fit Pvalue of 1.71. The experimental optimum yield recorded is 7.30 g with a standard deviation of 0.251. The XRF analysis reveals 71.415 % and 79.120 % silica in the rice husk and final silica respectively. The XRD results shows predominance of amorphous silica while the SEM image shows that the silica possesses agglomerates particles of irregular shapes that are jagged and porous. The elemental analysis from the EDX is in accord with the XRF result. The BET results showed that the silica has a surface area of 314 m²/g. pore volume of 0.1761 cm3/g and pore size of 2.128 nm. From all the results gathered, silica of significant quality and characteristics can be successfully produced from Bida rice husk.

Introduction

Optimization is an Engineering technique that can best be described as a complex mathematical approach that leads to identifying and selecting the best conditions from a set of probable design alternatives. Response surface methodology (RSM) is a powerful optimization tool that has been recognized for studying the interactions of two or more variables and optimizing the process parameters for efficient and profitable production of the product of interest (Olawale et al., 2013).

The utilization of non-renewable natural resources is currently increasing beyond imagination. This practice has a tremendous environmental negative impact (Bauma, 2019). As such, materials engineering which is the study of materials, their compositions.

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and their technological transformations into useful products should be given global emphasis to intensify researches on sourcing renewable raw materials in order to protect our environment and maintain sustainability (Aderemi et al., 2011).

Rice is the third ranked cereal produced globally with maize topping the list followed by wheat. However, considering world carbohydrate source, rice top the list of demand for the majority of the world population (Ummah et al., 2015). The annual global milled rice production stands at about 480 million metric tons. The leading rice producing countries are China and India accounting for about 50% of the rice cultivated and consumed. The consumption of rice per capita in Nigeria stand at \$2kg resulting to 4.7% increase a decade ago making the overall consumption of to 6.4 million tonnes in 2017 as against 3.7 million tonnes cultivated per year (Musa et al., 2024).

Environmental Pollution caused by waste deposition is a significant global problem. As a result of that, many researchers have diverted their attention towards waste management by way of minimizing them through recycling (Nayel et al., 2018).

Agricultural wastes are byproducts from the cultivation and processing of varieties of raw agricultural products that more often than not comprises of materials that can be transformed into useful products that are beneficial to man (Obi et al., 2016).

Rice husk is a by-product of rice milling produces rice husk which is an agricultural waste as a byproduct. The current global rice production of about 600 million tons/year invariably indicates that about 120 million tons of rice husk waste produced annually translating to about 20 wt % of overall rice production. The composition of rice husk is approximately 32% cellulose, 21% hemicelluloses, 22% lignin, and 15% mineral ash. On the other hand, the mineral ash is comprises of 55 to 97 % SiO₂, mixed with some minor constituents like K₂O, MgO, Fe₂O₃, CaO, and Al₂O₃ among others (Nayel et al., 2018). The compositions of the mineral ash varies due to the fact that the composition of the source rice husk depends on the variety of the rice from which the husk is obtained and the climatic and soil conditions of the location where it is grown (Seitkhan et al., 2019).

Rice husk are usually dumped haphazardly at dumping sites close to processing (milling) plants and afterward burnt into ashes after long time accumulation. This results into tremendous environmental nuisance and subsequent damage to the land and it's environs in which (Rajesh and Sounak, 2013)

Silica has wide range of applications as a basic raw material in the manufacture of semiconductors, ceramics, polymers, cement, solar panels and as a support in catalysts manufacture (Fernandes et al., 2017). The conventional method of manufacturing of crystalline silica industrially is based on physicochemical processes requiring high amount of thermal energy at high temperatures utilizing large amounts of acids couple amount of thermal energy at high temperatures utilizing large amounts of acids couple with the generation of large volumes of effluents as a waste. This method aside high energy consumption and discharge of significant quantity of liquid effluents it also release energy consumption and discharge of significant quantity of liquid effluents it also release

a significant quantities of greenhouse gases (Fernandes et al., 2017).

Since the compositions of a typical rice husk depends on many factors among which includes agricultural practices (amount and type of fertilizers used), soil composition and includes agricultural practices (amount and type of fertilizers used), soil composition and climatic or geographical factors. This particular research focuses on the optimization of

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amorphous Silica production from Bida rice husk using Response Surface Methodology (RSM) via a low temperature alkaline extraction process.

Optimization of the yield of silica from rice husk ash

- (i) Preliminary investigation of process parameters
 - 1. Effect of NaOH concentration on the yield of silica from rice husk ash; Exactly 10 g of rice husk ash produced at 700 °C was weighed and placed in 500 ml besker and 100 ml of 1.0 M NaOH was added to it. The mixture was then transferred to a constant temperature magnetic stirrer preset at 80 °C and speed of rotation 200 r.p.m. The reaction was allowed to proceed for a period of 1 hour. After the time allotted, the mixture was allowed to cool and filtered. The residue was discarded while the filtrate (sodium silicate solution) was titrated against 6.0 M tetraoxosulphate (IV) acid (H2SO4) until a pH of 7 was obtained. The resulting mixture was then filtered and the white residue (Silica) was collected washed severally with distill water and dried in an oven until a constant weight was obtained and recorded. The procedure was repeated by varying the NaOH concentration of 2.0, 3.0, 4.0 and 5.0 M and each time the weight of the final dried silica were recorded. Using the factorial method, the remaining parameters were investigated by varying them one after the other and keeping those investigated constant at values that gave the highest yields of silica
 - 2. Effect of volume of NaOH on the yield of silica from rice husk ash: The procedure in (1) was repeated using constant NaOH concentration of 3.0 M keeping all other parameters constant and varying the volume of NaOH using 150, 200, 250, 300 ml. After each experiment, the weight of the final dried silica was measured and recorded.
 - 3. Effect of reaction time on the yield of silica from rice husk ash: The procedure in (2) was repeated using constant NaOH concentration of 3.0 M and constant volume of NaOH of 250 ml keeping all other parameters constant. The reaction time was then varied from 30 to 180 minutes with step change of 30 minutes. After each experiment, the weight of the final dried silica is measured and recorded.
 - 4. Effect of reaction temperature on the yield of silica from rice husk ash: The procedure in (3) was repeated by fixing the NaOH concentration of 3.0 M, volume of NaOH 250 ml and reaction time of 120 minutes. The reaction temperature was then varied using 80, 90, 100, 110 and 120°C. The weight of silica was determined and recorded after each experiment
- (ii) Optimization of process parameters using response surface methodology

The results from the preliminary investigation were used to design the experiment and four (4) level factors which include NaOH concentration (A), volume of NaOH (B) the reaction time (C) and the reaction temperature and their levels were used for

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number runs and the software used is design expert 13.0 and a total of 29 the yield of silica by each run experimentally. The experimental results were again maximum yield of silica. The average silica yield obtained at the optimum suggested deviation.

Characterization of rice husk ash and silica produced

Both the rice husk ash and the silica produced are characterized using XRF, XRD, SEM/EDX and BET using standard methods. The oxides compositions of rice husk ash and silica produced were analyzed using Thermo fisher Scientific XRF analyzer (Model Number: ARL .QUANT'X. EDXRF analyzer). The XRD analysis of samples were determined using Rigaku Mini Flex 300. The SEM/EDX analysis was performed using PHENOM Scanning Electron microscope Model No; PRO:X:800-07443 Serial NO: MVE10570775

Results and Discussions

RSM Optimization of Silica Dissolution from Rice Husk Ash Preliminary Investigation

For purpose of optimization using response surface methodology, the major processing parameters that affect the dissolution of silica from rice husk (an agricultural waste found dumped in one of the major dumping site in Bida, Niger state in Nigeria) were put into experimentation so as to ascertain how the variation of each affects the yield and also to determine their upper and lower limits. The major parameters considered are: NaOH concentration, Volume of NaOH, reaction time and reaction temperature.

Effect of variation of NaOH concentration on the yield of silica from rice husk ash

Sodium hydroxide concentration affects the rate of its reaction with silica. As such, its variation will have significant effects on the yield of silica. This is tested by varying the NaOH concentration using 1.0, 2.0, 3.0, 4.0 and 5.0 M. The result obtained is showed in figure 1

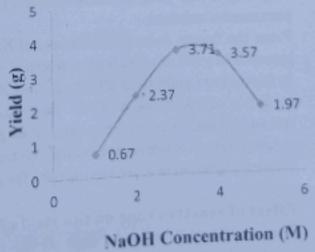


Figure 1: Effects of NaOH concentration on the yield of silica from 10 g of rice husk ash

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As expected as the concentration of NaOH is increased from 1.0 to 3.0 M the yield of silica increases steadily from 0.67 to 3.71 g corresponding to percentage yields of 6.7 to 37.1 % after which the yield declined with corresponding values of 3.57 and 1.97 g equivalent to 35.7 and 19.7 % yields for NaOH concentrations of 4.0 and 5.0 M respectively. The decline in yield may be as result of larger number of molecules of NaOH in solution that results in more collusion between same molecules of NaOH than between them and the silica contents of the ash. This will subsequently leads to lower rate of reaction and lesser yield

Effect of volume of NaOH on the yield of silica from rice husk ash The volume of the base has a significant role on the heterogeneous reaction since the liquid part of the reactant is expected to be absorbed into the solid ash to reach on to the silica before

reaction takes place.

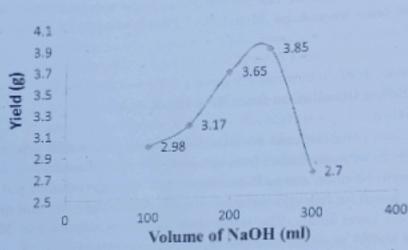


Figure 2: Effects of volume of NaOH on the yield of silica from 10 g of rice husk ash

For this reason, the greater the volume the more mobile and the chance of the NaOH molecules to penetrate into the solid ash and react with the silica. Figure 2 shows the

response of the yield of silica to the variation of the volume of NaOH keeping other parameters constant.

From the figure, increase in volume of NaOH from 100 to 250 ml recorded a significant increase in yield of silica with numerical value of 2.98 to 3.85 g corresponding to increase in percentage yield from 29.8 to 38.5 %. At a higher volume of 300 ml the yield declined to 2.7 g (27.0 % yield w/w). The decline in yield is associated with increase in intermolecular spaces within the NaOH molecules in solution which subsequently leads to lower rate of collusion between its molecules and that of the solid ash. Therefore, NaOH volume of 250 ml is more appropriate for silica dissolution from the ash.

Effect of reaction time on the yield of silica from rice husk ash

The significant of reaction time on the yield of silica was investigated by varying the reaction between 1 to 3 hours with a step change of 30 minutes. The result of such investigation is presented in Figure 3

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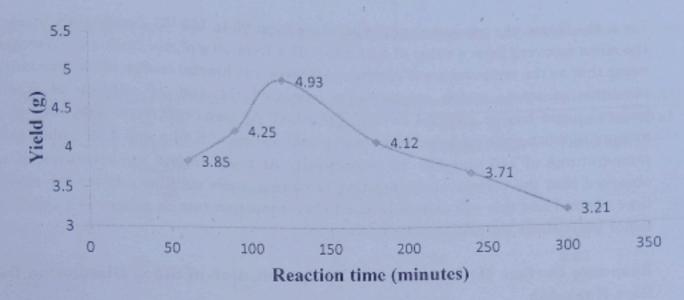


Figure 3: Effects of reaction time on the yield of silica from 10 g of rice husk ash

From Figure 3, as the reaction time rises from the initial time of 60 to 120 minutes the yield of silica increases from 3.85 to 4.93 g corresponding to 38.5 to 49.3 % yield w/w. As the reaction time goes beyond 120 minutes, the yield declined gradually with time. This may be attributed to the fact that longer reaction time results in lower reaction volume due to evaporation. The time of 120 minutes (2 hours) is the maximum reaction time for silica dissolution from rice husk ash.

Effect of reaction temperature on the yield of silica from rice husk ash

Temperature being an important factor that affects the rate of reaction was tested to see how it affects the recovery of silica from rice husk ash. For this investigation the reaction temperature was varied between 80 to $120\,^{\rm o}$ C using a step change of $10\,^{\rm o}$ C. The result of this test is presented in Figure 4

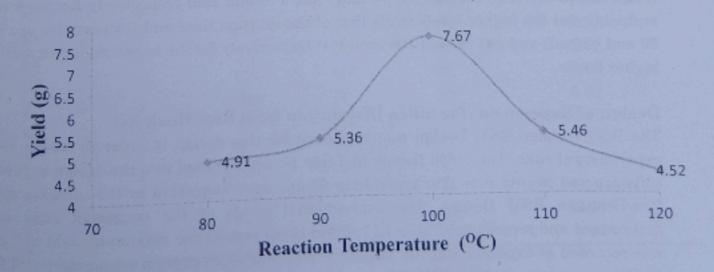


Figure 4: Effects of reaction temperature on the yield of silica from 10 g of rice husk ash

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From the figure, the increment of temperature from 80 to 100 °C significantly increases the silica recovery from a value of 4.91 g to 7.67 g from 10 g of rice husk ash. The reason being that as the temperature of reaction increases, the kinetic energy of the molecules of reactants increases which subsequently increased the rate of collision of reacting molecules and lead to increase in rate of reaction. At temperatures beyond 100 °C, the amount of silica recovered declined with specific values of 5.46 g and 4.52 g obtained at temperatures of 110 and 120 °C respectively. At these higher temperatures, it was observed that the volume of the reacting mixture reduces significantly for the reaction time allotted and this will definitely lead to lower reaction rate as volume is a significant factor that affects the rate of silica recovery.

Response Surface Methodology (RSM) Optimization of Silica Dissolution from Rice Husk Ash

The results of the preliminary investigations of the independent variables were used to generate the values in Table 4.16 consisting of four factors with their levels (lower, midpoint and higher values).

Table 1: Factors and their levels for Box-Behnken Design for silica dissolution from rice husk ash

Variable	Symbol	Co	oded Factor	levels
e e		-1	0	+1
Concentration of NaOH	A	1.0	1.5	3.0
Volume of NaOH	В	100	175	250
Reaction time	C	60	90	120
Reaction Temperature	D	80	90	100

From Table 1, the coded factor levels for the concentration and volume of NaOH temperature are (1.0, 1.5 and 3.0 M) and (100, 175 and 250) respectively for the lower, midpoint and the higher levels while that of the reaction time and temperature are (60, 90 and 120 ml) and (80, 90 and 100 minutes) respectively for the lower, midpoint and the

Design of Experiment for Silica Dissolution from Rice Husk Ash

The Box-Behnken RSM Design was suggested for this design in order to obtain lower experimental runs. The coded factors in Table 1 were imputed into the design expert 13 software and twenty nine (29) experimental runs were suggested by the software using Box-Behnken RSM Design. The experimental yields of the suggested runs were determined and recorded in Table 4.17. From these results the maximum yield of 7.21 g was recorded at experimental run twenty five (25) at experimental parameters of 3.0 M NaOH concentration, 250 ml NaOH volume, 60 minutes reaction time and 90 °C reaction temperatures while the lowest silica yield of 3.69 g was observed at run seventeen (17) at

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30 minutes reaction time, 80 $^{\circ}$ C reaction temperatures and 2.0 M NaOH with a volume of 175 ml.

Table 2: Experimental yields for Box-Behnken experimental design for silica dissolution

Std	Run	Factor (A) NaOH	Factor (B) Vol of	Factor (C)	Factor (D) Temperature (°C)	Experimental
		Conc. (M)	NaOH (ml)	(minutes)		
12	1	3	175	60	100	7.18
29	2	2	175	60	90	5.61
26	3	2	175	60	90	5.65
21	4	2	100	60	80	5.31
24	5	2	250	60	100	7.10
7	6	2	175	30	100	6.15
11	7	1	175	60	100	5.28
9	8	1	175	60	80	4.52
3	9	1	. 250	60	90	5.03
27	10	2	175	60	90	5.59
25	11	2	175	60	90	5.93
22	12	2	250	60	80	4.65
1	13	1	100	60	90	4.38
28	14	2	175	60	90	5.61
19	15	1	175	90	90	4.45
6	16	2	175	90	80	4.95
	17	2	175	30	80	3.69
5		2	250	30	90	4.70
14	18	2	100	60	100	4.53
23	19		250	90	90	5.57
16	20	2	175	30	. 90	5.89
18	21	3 .	175	90	90	6.45
20	22	3	100	60	90	6.02
2	23	3	100	90	90	4.55
15	24	2		60	90	7.21
	25	3	250	30	90	4.31
3	26	2	100	60	80	6.28
10	27	3	175	30	90	3.95
7	28	1	175		100	5.27
1	29	2	175	90		

From these results, it is evident that all the coded factors have a positive effect on the yield since an increase in any of the factors brings about an increase in the yield.

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Analysis of Results of Experimental Design for Silica Dissolution The results of the suggested experimental design in table 2 were analyzed by the software and compared with the predicted values. Tables 4.18-4.20 and Figures 4.13-4.19

del for optimization of silica dissolution from rice husk ash

Source	Sequential p-value	Lack of Fit	Adjusted R ²	Predicted R ²	
Linear	< 0.0001	0.0054	0.6235	0.5052	
2FI	0.0363	0.0104	0.7454	0.5064	
Quadratic	< 0.0001	0.3198	0.9654	0,9141	Suggested
Cubic	0.1154	0.7954	0.9828	0.9374	Aliased

From the fitted summary Table 3, the quadratic model was suggested as the most fitted model that describes the silica dissolution from rice husk ash. The quadratic suggested has a sequential P-value of < 0.0001, lack of fit P-value of 0.3198, adjusted and predicted \mathbb{R}^2 of 0.9654 and 0.9141 respectively.

The analysis of variance (ANOVA) was also generated and the result was presented in Table 4 From the results, the software suggested model F-value of 56.76 implies that the model is significant as there is only 0.01 % chance that F-value as large as this will occur due to disturbance.

Table 4: Analysis of variance (ANOVA) for silica extr

Source	Sum of Squares	df	Mean Consu		rice nus	Kasn
Source Model A-NaOH CONC B-Volume of NaOH C-Reaction Time D-Reaction Temp AB AC AD BC BD CD	Sum of Squares 24.29 10.87 2.22 0.5419 3.11 0.0729 0.0009 0.0049 0.0992 2.61 1.14	df 14 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Mean Square 1.73 10.87 2.22 0.5419 3.11 0.0729 0.0009 0.0049 0.0992 2.61	F-value 56.75 355.48 72.57 17.72 101.76 2.38 0.0294 0.1603 3.25 85.31	p-value < 0.0001 < 0.0001 < 0.0001 0.0009 < 0.0001 0.1448 0.8662 0.6949 0.0932	k ash significant
A ² B ² C ² D ² Residual Lack of Fit	0.2145 0.3377 2.80 0.0077 0.4280 0.3467	1 1 1 1 1 14 10	1.14 0.2145 0.3377 2.80 0.0077 0.0306 0.0347	37.45 7.01 11.05 91.56 0.2513	< 0.0001 < 0.0001 0.0191 0.0050 < 0.0001 0.6239	
Pure Error Cor Total	0.0813 24.72	4 28	0.0203	1.71	0.3198	not significant

The model term with P-values less than 0.0500 indicate that those model terms are significant while those with P-values greater than 0.1000 are not significant model terms.

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Following these criteria, the model terms A, B, C, D, BD, CD, A2, B2, and C2 are significant model terms while AB, AC, AD, BC and D2 are the insignificant model terms. The lack of fit F-value of 1.71 is considered not significant and therefore suggests that the model well fitted the experimental results. This F-value of 1.71 signifies that there is only 31.98 % chance that this value could occur due to disturbance.

Table 5 contains the result of the model fit statistics. The result showed the predicted R2 of 0.9141 is in agreement with the adjusted R2 value of 0.9654 since the difference between the two is less than the maximum prescribed value of 0.2. The adequate precision which is a measure of signal to disturbance ratio, suggests that the ratio should not be less than The obtained ratio of 28.5582 signifies an adequate signal or precision.

Table 5: Model Fit statistics for silica dissolution from rice husk ash

		R ²	0.9827
Std. Dev.	0.1749	Adjusted R ^a	0.9654
Mean	5.37	Predicted R*	0.9141
C.V. %	3.25	Adeq Precision	28.5582

The R³ value of 0.9865 from this particular research is greater than the value of 0.8454 reported by (Adepoju et al., 2019) for the same African pear seed oil using Box-Behnken RSM Design. When the fit statistics was also compared with that of the work reported by Musa et al. (2016) using central composite RSM design for the extraction of Avocado pear seed oil the standard deviation of 0.1749 from this particular research is better than the value of 1.12 reported by Musa et al. (2016). The R2 value of 0.9827 from this research is better than 0.9211 and 0.8454 reported by Musa et al. (2016) and Adepoju et al., (2019) respectively. The adjusted R2 of 0.9654 and the adequate precision of 22.0787 recorded from this work are better than the values of 0.8648 and 13.016 respectively reported by

The equation suggested for silica dissolution from rice husk ash by the software in terms of the coded factors is presented as equation 1

 $Yield\ (Y) = +5.68 + 0.9517 A + 0.4300 B + 0.2125 C + 0.5092 D + 1350 A B + 0.0150 A C + 0.0350 A D + 0.0150 A C + 0.000 A C$ $+0.1575BC+0.8075BD-0.5350CD+0.1818A^2-0.2282B^2-0.6569C^2-0.0344D^2...(1)$ Eliminating the insignificant model terms from the ANOVA Table 4, which are: AB, AC, AD, BC and D2, the final model equation for the optimum yield of silica is represented by equation (2)

Equation 2 can be useful in predicting the response (yield) of any given level of each factor in the equation. In that regard, the equation can be used for identifying the relative impact of the factors by comparing the factor coefficients.

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Interactions of Process Parameters

The software plotted predicted silica yield against actual yield and the graph in Figure 5 was obtained. The plot shows that the residuals follow a normal distribution (Umeuzuegbu, J. C et al., 2020)

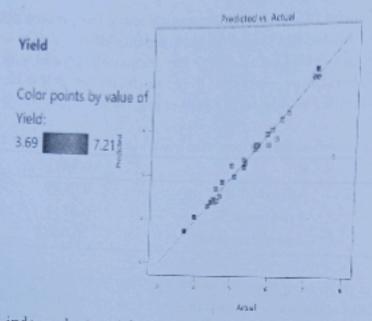
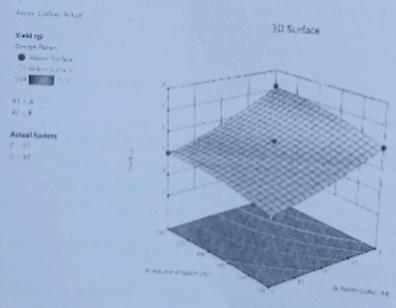


Figure 5: Plot of predicted against actual yield of silica The points in the graph are closely distributed along the straight line of the plotted graph which is a testimony of the close relationship between experimental yields and the vields. The predicted confirms that the response variables in the experimental results are adequately predicted by the model.

The 3D response plots shows the interactions among

independent variables by showing the effects of combination of the variables on the yield of silica extracted from the rice husk ash. Figure 6 depicts the interaction between the volume and concentration of NaOH solution and both factors has positive effect on the oil



their highest yield of 7.21 g silica.

Figure 6: Response surface plot for the interaction between the volume and NaOH concentrations The lowest yield was recorded by their lowest values of their interaction (100 ml and 1.0 M) is 4.38 g silica while the interaction of their higher values of 250 ml volume of NaOH and 3.0 M NaOH concentration produce

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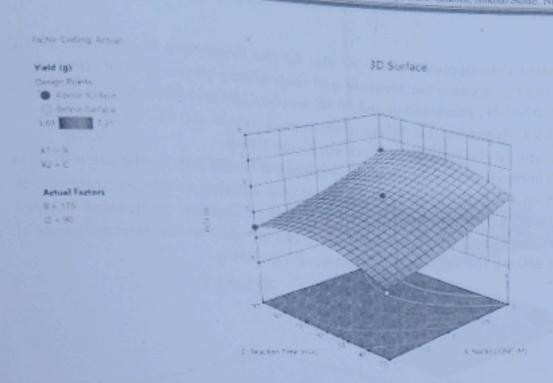


Figure 7: Response surface 3D plot for the interaction between reaction time and NaOH concentration

The interaction between the concentration of NaOH (A) and the reaction time (C) also has direct proportional effect on the yield in the sense that increase in both parameters results in increase in the silica yield as presented by Figure 7. The Figure shows that at the lower values of these parameters which are: 1.0 M NaOH and 30 minutes reaction time, the yield of silica recorded was the lowest recorded throughout the research with a numerical value of 3.95 g silica. Considering the interaction of their higher values of 3.0 M NaOH concentration and 90 minutes reaction time the yield recorded was 6.45 g silica.

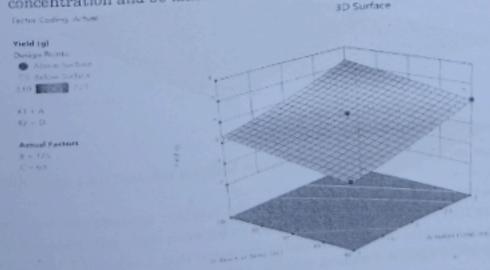


Figure 8: Response surface 3D plot for the interaction between the NaOH concentration and reaction temperature

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Figure 8 represent the response surface 3D plot for the interaction between the NaOH concentration and the reaction temperature and their effects on the yield of silica. From the Figure, at 1.0 NaOH concentration and 80 °C reaction temperatures, the yield of silica obtained was 4.5 g. At the highest values of these parameters (3.0 M NaOH and 100 °C reaction temperatures) the yield of silica recorded was 7.18 g.

The interaction between the reaction time and volume of NaOH follows the same trend of positive impact on the yield when both are increased simultaneously as presented in Figure 9. From the Figure, it can be seen that the lowest yield of 4.31 g silica was recorded at the lowest interaction values of 30 minutes and 100 ml while at the extreme values of $90 \mathrm{\ minutes}\ \mathrm{and}\ 250 \mathrm{\ ml},$ the yield of silica registered was $5.57 \mathrm{\ g}.$

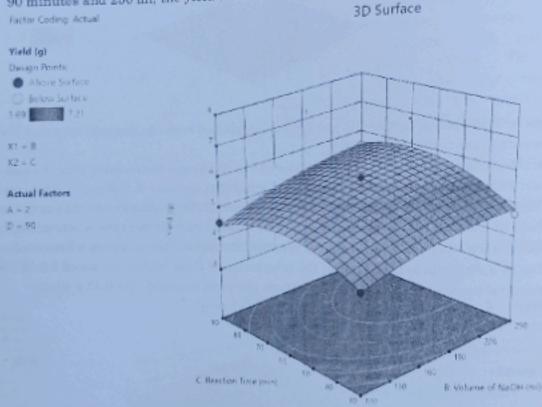


Figure 9: Response surface 3D plot for the interaction between reaction time and volume of NaOH

The interaction between the volume of NaOH and the reaction temperature was well described by Figure 10. From the Figure the interaction between these parameters has a significant impact on the yield of silica obtained in the sense that a value of 7.10 g silica yield was recorded at the highest parameter values of 250 ml and 100 °C while the yield of 5.31 g silica was recorded at the lower values of these parameters.

When the interaction between the reaction time and the reaction temperature are observed, the behaviour of the yield of silica was well represented by Figure 11

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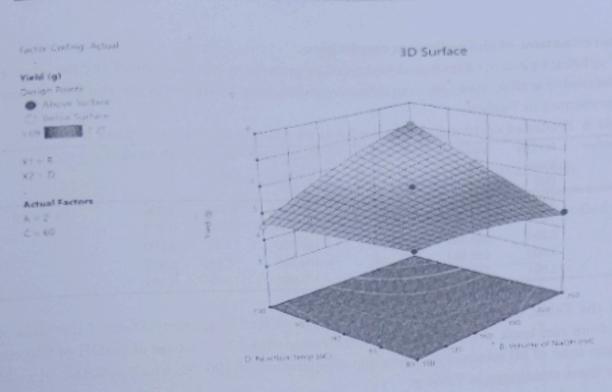


Figure 10: Response surface 3D plot for the interaction between volume of NaOH and reaction temperature

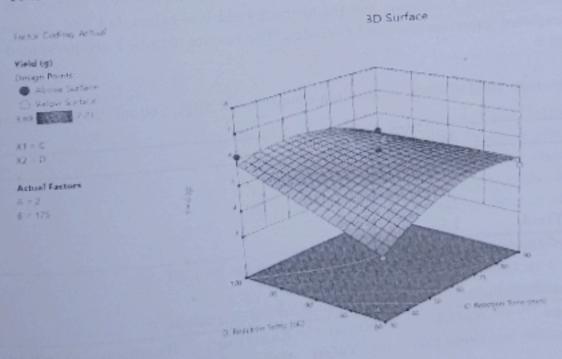


Figure 11: Response surface 3D plot for the interaction between reaction time and reaction temperature. From the Figure, the lower values of 30 minutes reaction time and 80 °C produced a lower yield of 3.69 g while a higher yield of 5.27 g silica was recorded at 90 minutes and 100 °C.

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Determination of the optimum conditions The optimum yield of silica was determined at maximum combination of the parameters onsidered. For this, about 85 solutions were carried out by the software and the best five are presented in Table 6

ditions for silica dissolution from rice husk ash

Number	NaOH Conc	Volume of NaOH	Reaction Time (Minutes)	Reaction Temp (°C)	Yield (g)	Desirability	
1 2	(M) 3.000 3.000	(ml) 250,000 249,395	90,000	100.00 100.000	7.655 7.650	1.000 0.999	Selected
3 4 5	2,991 3,000 3,865	250.000 249.983 248.566	89.996 89.426 89.993	100.000 100.000 100.000	7.645 7.686 7.638	0.999 0.998 0.998	

From the Table, the optimum conditions suggested for the maximization of the yield of silica from rice husk ash are: NaOH concentration of 3.0 M, Volume of NaOH of 250 ml. reaction time of 90 minutes and reaction temperature of 100 °C. The predicted oil yield under these conditions is 7.655 g.

Validation

For the validation of the model suggested, three set of experiments were carried out at the suggested optimum conditions and the average yield was calculated and compared with the predicted value via standard deviation. The results obtained are presented in Tables 7and 8

Table 7: Average yield of silica at optimum conditions of 3.0M, 250 ml, 90 minutes and

Run	APSO Yield (g)	
1	7.25	
2	7.12	
3	7.53	
Average Yield	7.30	

ble 7 the average yield of silica was calculated to be 7.30

Table 8: Standard deviation for optim

Parameters	NaOH Conc (M)	of NaOH	Reaction time (min)	Reaction	Yield (g)
Optimum value Validation value	3.0	(ml) 250	90	Temp(°C)	
Standard	3.0	250	90	100	7.655
deviation				100	7.300
		Marie Control			0.2510

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From Table 8, the result of the predicted optimum yield was compared with the experimental average value and the standard deviation was found to be 0.2510. This low the actual experimental results.

Characterization of Rice Husk Ash and Silica Produced Fourier Transform Infrared Spectrograph (FTIR) of Rice Husk Ash

Figure 12 show the FTIR spectrum of rice husk ash. From the figure, about seven peaks were identified. Considering the single bond region, two peaks were identified with the

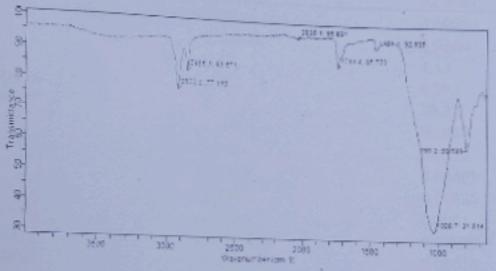


Figure 12: FT-IR Spectrum of rice husk ash

Wave number 2922.2 cm⁻¹ and this indicates the presence of -CH₃ (Methyl) group from a saturated aliphatic compound with a C-H stretch vibration. This is in agreement with the report of Melis et al., (2022) for rice husk ash. The second peak at this region was observed at 2855.1 which signifies the presence of a methylene (-CH₂) group also from a saturated aliphatic compound with a C-H symmetrical stretch vibrations (Asep et al., 2019) and this is in conformity with the report of Melis et al., (2022).

Within the triple bond region, the peak found at a wave number of 2035 cm⁻¹ indicates the presence of a cyanide or thiocyanide ions (Asep *et al.*, 2019) and at a wave number of 1744.4 cm⁻¹, indicates the presence of carbonyl group C=O and this is in agreement with the report of Melis *et al.*, (2022) for rice husk ash produced at 300 °C.

Among the components dictated at the finger print region are carbonate (CO3-2) and silicate

(SiO₂-2) ions at wave numbers of 1451.1 and 790.2 cm⁻¹ respectively (Asep *et al.*, 2019). The last wave number of 1028.7 cm⁻¹ in this region signifies the presence of organic silicon with Si-O-Si vibration and this is also in agreement with the reports of Daffalla *et al.* (2019) and Melis *et al.* (2022) respectively.

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Fourier Transform Infrared Spectrograph (FTIR) of Silica FTIR analysis was carried out on the silica sample produced and the FTIR spectrum of such analysis is presented in Figure 13. From the Figure it can be deducted that six peaks were identified one from the single bond region (4000 - 2500 cm⁻¹), two from the triple bond region (2500 - 2000 cm-1) and three within the finger print region.

At a peak of 3391.9 cm⁻¹ and transmittance of 93.29, Si-OH group was noticed and this is in agreement with the findings reported by Daffalla et al., (2010). The transmittance of 98.256 and wave number of 2165.6 cm-1 indicates the presence of cyanide ions or thiocyanide ions (Asep et al., 2019).

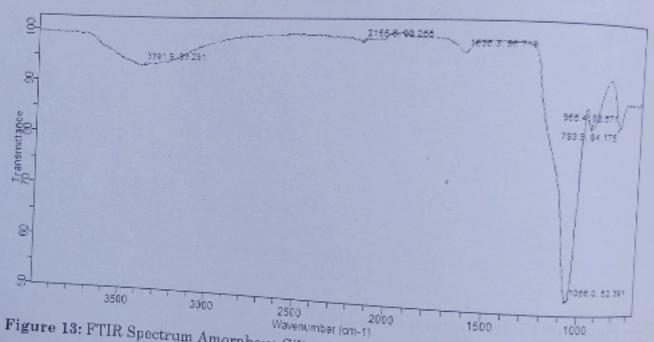


Figure 13: FTIR Spectrum Amorphous Silica

The wave number of 1836.3 cm⁻¹ and transmittance of 96.719 indicates the presence of an anhydride from a carbonyl compound with a functional group of C=O which is also in agreement with the report of Melis et al., (2022) and Daffalla et al., (2010) for rice husk

The peak at a wave number 965.41 cm⁻¹ and transmittance of 88.671 signifies the presence of silicate ions and this is also in line with the of silicate ions and this is also in line with the report of Melis et al., (2022) and Daffalla et al., (2022) and Daffalla et al., (2023) and al., (2010) for rice husk ash. An aliphatic chloro-compound containing a C-Cl stretch of 1066.0 cm⁻¹ signifies the presence of the last peak at a wave number of 1066.0 cm⁻¹ signifies the presence of phosphate ions.

XRF Analysis of Rice Husk Ash and Silica

The oxides compositions of both the rice husk and silica produced were carried out in other to observe the change in chemical composition. to observe the change in chemical compositions that follows after the treatment of the ash with NaOH solution and the precipitation of all with NaOH solution and the precipitations that follows after the treatment of the acid. The results of the XRF analysis is presented. acid. The results of the XRF analysis is presented in Table 9

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Table 9: XRF analysis of rice husk ash and silica produced

Oxides	Rice husk ash (%)	Silica (%)
Fe ₂ O ₃	0.4290	0.01366
CuO	0.02630	0.00676
ZnO	0.06302	0.01640
Ga ₂ O ₃	0.000254	0.000082
GeO ₂	0.000318	0.000533
CeO ₂	1.2294	1.2713
Eu ₂ O ₃	0.000447	0.00004
Lu ₂ O ₃	0.000023	0.00001
Ta ₂ O ₅	0.0029	0.00276
WO ₃	0.01306	0.01004
MgO	4.42	1.44
Al ₂ O ₃	1.863	0.983
SiO ₂	71.415	79.12
P2O5	3.295	0.1857
SO ₃	0.1304	0.0279
Cl	0.0128	0,00865
K ₂ O	1.4563	0.00825
CaO	0.7224	0.2051
TiO2	0.05860	0.00660
V ₂ O ₅	0.00195	0.00016
Cr ₂ O3	0.00079	0.00011
MnO	0.3509	0.00267
BaO	0.02572	0.01609
Ae ₂ O ₃	0.0006	0.0009
	0.000039	0.000168
Br	0.01206	0.000084
Rb ₂	0.0076	0.03000
ZrO:	0.00178	0.00059
РЬО	0.02513	0.02434
Bi ₂ O3	0.000402	0.000494
Ag ₂ O	0.000540	0.0000
I	0,000040	

From the Table, the composition of silica in the rice husk ash produced at 800 °C was 71.415 %. This value is in close agreement with the report of Taku et al., (2016) with a value of 73.20 % silica from the ash produced at the same temperature of 700 °C but lower than 84.4 % and 83.8 % reported by Seitkhan et al., (2019) for rice husk ash produced at 700 °C from an untreated rice husk. These disparities may be attributed to the fact that the composition of rice husk ash depends on the variety of the rice from which the husk is obtained and the climatic and soil conditions of the location where it is grown (Seitkhan et al., 2019). After the chemical treatment of the ash, the sample of silica obtained was

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79.12 % pure, this value is less than 98.2 % silica produced from rice husk treated with HCl prior to ashing as reported by Seitkhan et al., (2019) and 99.9 % silica reported by Ezzat et al., (2012) for nano silica produced from acid pretreated rice husk. The discrepancies in the purity of the final silica is due to initial compositions of the different varieties of the rice husk used and the pretreatment carried out on the husk prior to silica production from the ash (Seitkhan et al., 2019). From the table, composition of other constituents of the ash diminishes during the course of silica production.

XRD analysis of rice husk ash

The XRD spectrum of rice husk, as presented in Fig. 14, indicates a broad peak at 20 of 22.23° which is attributed to amorphous silica. A sharp reflection peak at 2θ of 26.98° corresponds to the crystalline silica. Therefore, the prominent peaks in the rice husk ash indicate a combined amorphous and crystalline silica phase. The formation of the sharp and intense peak of silica starts to form at ≥750 °C (Ana Maria et al., 2009), while at low temperatures (≤700 °C), the broad peak observed is amorphous (Ezzat et al., 2012).

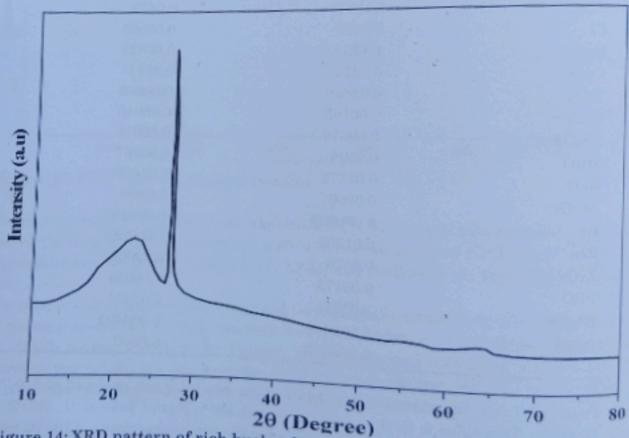


Figure 14: XRD pattern of rich husk ash produced at 700 °C

XRD analysis of amorphous silica

XRD analysis for amorphous silica is represented in Fig. 15. A reflection peak at 2θ of 130 / Page

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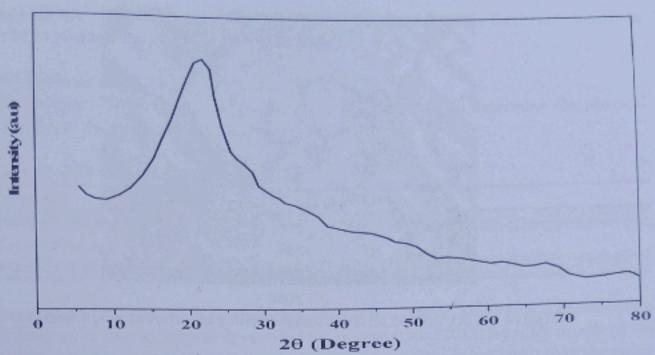


Figure 15: XRD analysis of amorphous silica

At temperature >500 °C and ≤ 700 °C is responsible for the formation of amorphous silica (Ana Maria et al., 2009). The amorphous structure of silica will allow the formation of a polymeric structure with a hydroxyl group, leading to the existence of a silanol group via a covalent bond with Si (Si-O-H) (Ngoc et al., 2018).

SEM/EDX Analysis

SEM/EDX analysis was carried out in order to determine the structural morphology and the elemental compositions of the silica produced. The results of such analysis are presented in figure 16 and table 10 for SEM and EDX respectively.



(a) 500 ×



(b) 1000 ×

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(C) 2000 ×

Figure 16: (a), (b) and (c) SEM image of silica at different magnification

Table 10: EDX Analysis of Silica			Atomic	Weight
Element Number	Element Symbol	Element Name	Conc.	Conc.
13	Al	Aluminium	1.36	1.30
20	Ca	Calcium	0.34	0.48
26	Fe	Iron	0.24	0.48
11	Na	Sodium	0.52	0.42
16	S	Sulfur	0.26	0.30
-19	K	Potassium	0.14	0.19
17	Cl	Chlorine	0.14	0.17
12	Mg	Magnesium	0.00	0.00
22	Ti	Titanium	0.00	0.00
25	Mn	Manganese	0.00	0.00
15	P	Phosphorus	0.00	0.00

The SEM image in figure 16 (a), (b) and (c) represents monograms of the morphology of silica produced at optimum conditions viewed at different magnifications of 500 \times , 1000 \times and 2000 × respectively. From the images, it can be seen that the silica possesses agglomerates particles of irregular shapes that are jagged. This finding is similar with the report of Iara et al., (2017). The surface of the silica as observed from figure 16 (c) with 2000 times magnification is found to possess significant developed pores which may be due thermal treatment of the husk during the generation of the source ash. Similar observation was reported by (Olawale et al., 2013).

Table 10 shows the results of the EDX analysis of the Silica produced. The silicon composition of 97.01 % is an evidence of predominance of silica in the final product. When

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compared with the XRF results in table 9, this composition of silicon further authenticate the 79.12 % silica composition in the final product.

BET Analysis of Silica

BET analysis was performed on the produced silica in order to determine the physical properties of the silica and the result is presented in table 11

Table 11: BET Physical properties of Silica

Property	Value	
Surface Area (cm²/g)	314.0	
Pore Volume (cm³/g)	0.1761	
Pore size(nm)	2:128	

From the table, the BET surface area is recorded to be 314m²/g. This value is greater than 186.5792 m²/g and 68.2269 m²/g reported by Nguyen et al., (2018) for silica produced via Alkaline extraction and SiO2 precipitation methods respectively but lower than the value of 980 m2/g reported by Seitkhan et al., (2019) for silica produced from rice husk ash obtained from Hcl pretreated rice husk. It is also lower than value of 623 m²/g reported by Ezzat et al., 2012 for nano silica produced from rice husk ash. The pore volume of 0.1761 cm3/g recorded in this research is lower than 1.2 cm3/g reported by Seitkhan et al., (2019) and greater than 0.02408 cm3/g reported by Ezzat et al., 2012. The pore size of 2.128 nm registered is greater than 0.9 nm reported by Seitkhan et al., (2019).

Conclusion

Pure white amorphous silica was successfully produced and optimized using RSM from Bida rice husk. A quadratic model was suggested and the analysis of the model shows that it has an insignificant P-value of 1.71 which suggests that the model well describe the experimental results. The model fit statistics also shows that the predicted R2 value of 0.9141 is in agreement with the adjusted R2 value of 0.9654. The adequate precision of 28.5582 ≥ 4 indicates that the model is précised. About 73.0 % yield of silica was achieved from the ash at optimum conditions. The results of the yield and characterization of the products were very much comparable with most of the report of the findings in the literature.

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