ELECTROPLATING OF FERROUS METAL USING MIXTURE OF ELECTROLYTES

By

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DECEMBER, 2005.

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A RESEARCH PROJECT SUBMITTED TO THE DEPARTMENT OF CHEMICAL ENGINEERING SCHOOL OF ENGINEERING AND ENGINEERING TECHNOLOGY, FEDERAL UNIVERSITY OF TECHNOLOGY, MINNA NIGER STATE, NIGERIA. IN PARTIAL FULFILLMENT OF THE REQUIREMENTS FOR THE AWARD OF BACHELOR DEGREE IN ENGINEERING (B. ENG.) IN CHEMICAL ENGINEERING.

DECEMBER, 2005.

DECLARATION

I, Akuewulu. B. Ifeanyi, with matriculation number 2000/10610EH, declare that this thesis; electroplating of ferrous metal using mixture of electrolytes; has not been presented for the award of bachelor of engineering in chemical engineering else where.

12/17/05

Signature

Date

CERTIFICATION

This is to certify that this project titled "Electroplating of ferrous metal using mixture of electrolytes" was supervised, moderated and approved by the following underlisted persons on behalf of the Chemical Engineering Department, School of Engineering and Engineering Technology, Federal University of Technology, Minna.

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Date

External Examiner

Date

DEDICATION

dedicate this project to Almighty God, who made it possible for the successful completion of my Chemical Engineering Degree Program.

ACKNOWLEDGEMENT

I wish to acknowledge the grace of God Almighty in my life, for sparing my life throughout my course of study and successful completion of my first degree.

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ABSTRACT

Electroplating is the process of electro-deposition by which a thin smooth sound metallic deposit produced over the base metal. The objective of the experiment was to beautify, protect, insulate, or to increase corrosion resistance and surface properties of the base metal. In the experiment, a mixture of Sodium Cyanide, Zinc Cyanide, Sodium Hydroxide and brightener was used as the electrolyte. The zinc metal was used as the anode while the base metal is (iron bolts) made-up the cathode. With the aid of rectifier, a direct current is supplied to the electroplating bath which was used to plate 27 pieces of the work piece or the base metal. Using different values of voltage, current and time, the mass deposited at the base metal was determined with the corresponding thickness of the deposit. The best result was achieved using 1.4volts, 1.5Amps, and plating time of 9 minutes, to produce a mass deposit of 0.270g with a corresponding thickness of 1.84x10⁻³ cm. The surface properties and corrosion resistance of the base metal was improved to a considerable value at the end of the experiment.

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1.0 INTRODUCTION

The relation between chemical and electrical phenomena was investigated by M. Lomonov as early as in the middle of 19th century. He made much progress in the study of electrolyte solution. In 1853, I. Hillorf establishes that ions in a solution, in an electric field moves at different velocities determined by the nature of the ions. In 1874, F Kohidausch established the law of independence of electric conductivities of ions. In 1887, the Swedish scientist S. Arrhenius formulated the theory of electrolytic dissociation, which remains useful at the present time. In 1891. Kablukor (Ankeren, 1993) noted that Arrhenius theory must be used in combination with Medeleevis hydrated theory and pointed out that ions formed in molecular dissociation becomes hydrated. In 1923, strong electrolytes were invented. The work of the Soviet scientists, advanced to a considerable extent. Developing the concept of the theory of electrolysis. The development of theoretical concept of electrochemistry was accompanied by practical electrochemical process.

In 1805, Michael Faraday discovered the quantitative laws with reference to the amount of substances formed at the electrodes which depends on the quantity of electricity passed through the system. In 1838, Russian academicians, B. Yakobi used an electric current and metal deposited on different shaped electrode to obtain different metal articles. Yakobi's discovery subsequently gives birth to a new field of applied electrochemistry.

It also involves preferential or selective discharge of ion in an electrolyte, which depends on the position of the ion in the electrochemical series, concentration of the ion in the electrolyte and the nature of electrode. Electrolysis is defined as a chemical decomposition of a substance when an electric current is passed through it. The substance that decomposes is called an electrolyte and it is usually an acid, base or salt that conducts electricity when in solution or in molten from. Science of electroplating has been developed from this principle, if a direct current passed through an electrolyte, metal will be eaten away from the anode; the composition of the electrolyte remains unchanged. (Graham .A et'al)

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Electroplating beautifies, protects, insulates, or increases the corrosion resistance, conductivity or solderability of metal objects, generally of iron or copper alloys, but sometimes other metals as well.

The process involves dissolving metal at the anode and depositing it at the cathode. Direct current applied between the electrodes is conducted through the solution containing metallic salts. Because the ions depleted by the plating process at the cathode are replenished at the anode. The process is essentially self maintaining.

1.1 Summary of how Electroplating Works									
Anode	+	Metal ball or slabs are placed in a weekly acid or alkaline							
		solution. The acid or base helps the metal dissolve. The metal in							
	solution is in ionic form. An electric current passes through the								
solution causing the metal ion to gain electrons and cau									
		object to be plated.							
		To attract a coating of the metal in solution. The solution usually							
		also contain one or more wetting agents and gain refiners which							
Cathode	-	produce an attractive plated finish.							

Electroplating is the techniques by which solid metals is deposited on different articles to render their surface specific properties. Electroplating is the process whereby an object usually metallic is coated with one or more relative thin smoothly adherent layer of other metal. Electroplating is need when there is a need for surface characteristics that the base metal, selected for structural reasons does not posses. Electroplating protects, beautifies, insulates, or increases the corrosion resistance, conductivity or solderability of metal objects as well.

Electroplating was originally introduced as a means of applying a deposit of nickel, gold, or silver as a decorative finish to jewellery, cutlery and bicycle spare parts. It was the mastery of

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the science of British, German and American manufacturers and consequent superiority of their product that brought about the limelight of electroplating industry. Now, it has been developed to such an extent that there is hardly a branch of industry, which does not make use of the process, not only as a means of adding finishing to a product, but also to add a protective coating such as cadmium plating and anodizing. Common examples of electroplated materials are chromium plated steel for automobile accessories. Tin-plated steel for food containers and silver plated table wares such as spoon, forks, knives, gold plated jewellery and chromium plated automobile. The metal to be plated as well as the plating material is usually metal. Plating operation is important and necessary part of the manufacturing process and should be planned with the same care accorded to fabrication operations.

Electroplating works with the principle of electrolysis i.e. the reaction at the anode (anode half reaction) and at the cathode (cathode half reaction), which are oxidation and reduction (redox) reactions.

1.2 Aim and Objectives

The major objective of the project (zinc plating using alkaline bath) :

- 1) To get improve surface appearance on the basic metal
- 2) To obtain improved resistance to corrosion, tarnish, chemical and wear.
- 3) To increase hardness of metal
- 4) To increase electrical conductivity.
- 5) To change the surface properties of the metal
- 6) To beautify the surface or appearance of the metal.

1.3 Scope of Work

n theory at least to every metal, electroplating can occur and their electro-deposition can heoretically carried out. In practice however, there are chemical, electrochemical and netallurgical consideration, which considerably limit the number of metals with which the present state of knowledge can be difficult to electroplate, even impossible to plate.

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The process is based on the fact that when a direct current of electricity is passed between electrodes immersed in solution containing metallic salts, electrolysis will occur. This will result in metal ion migrating to the cathode.

2.0 LITERATURE REVIEW

2.1 An Overview of Electroplating

Electroplating is a process of electro deposition by which a thin smooth sound metallic deposit is produced over a basic metal. Electroplating protects, beautifies, insulates or increases the corrosion resistance, conductivity or solderability of metal objects, generally of iron or copper alloys, but sometime other metals as well. The process involves dissolving metal at the anode and depositing it at the cathode. Direct current applied between the electrodes is conducted through the solution containing metallic salts. Because the ions depleted by the plating process at the cathode are replenished at the anode, the process is essentially self-maintaining. (J. J. Moore)

Modern electroplating is as skilled as an operation of any other manufacturing endeavour. Plating baths, load size and current density are carefully controlled. Platers immerse objects into a series of chemical baths in order to change their surface conditions. The number of tanks and their chemical make-up differs based on the desired result and every plating plant is different.

Designers of goods to be finished need broader understanding of the processes used. Plates must know what kind of metal they are finishing. Every metal requires a somewhat different pre-treatment. Aluminium, for example, may dissolve in a solution designed for clearing steel. Even variation between alloys will require modification of the pre-treatment process. An incorrect identification may result in damage or even the destruction of the parts.

Metals pre-treatment or preparation is crucial because it affects adhesion and appearance, as well as, composition and properties of the final deposit. Platters need accurate information about pre-existing contamination, such as, inclusion, in the base metal, cutting oils used and any organic or inorganic surface films. Environmental regulations have severely restricted clearing options. While the choices are limited, most soils can be safely removed if the platters know what they are dealing with. Information supplied by the customers is the key to successful metal finishing. (Raymond Chang)

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1. 1 Principle of Electrolysis

lectrolysis is defined as gradual decomposition of a metal in an electrochemical cell when an ectric current is passed through it. Electrolysis was found by Michael faraday, who in the 870s and 1880s was the first person to investigate electrolysis systematically.

ften the Faraday written as a round number, perhaps 965000cmol⁻¹, which is not an ccurate but handily in calculation. (Philip Mattew)

here are many uses of electrolysis namely:

- 1) It is used in extraction of very reactive metal such as sodium
- 2) It is used in purification of metals containing impurities.
- 3) Electrolysis is also used to decompose compounds, and to convert them into more useful and valuable chemicals.
- 4) It can also be used in electroplating of metals to prevent wearing away of the metal which is mainly emphasized in this research.

In electrolysis, current is passed through a solution containing ions, or a molten salt, called the electrolyte. The negative electrode called the cathode is coated with electrons, some of which can be stolen by the positive ions that come close to the electrode.

A typical example of the reaction. (W. Kann et al)



2.2.0 Electrolysis of Molten Sodium Chloride

In the electrolysis of molten sodium chloride, sodium ions travel to the cathode and the sodium metal is liberated.

$$Na^+ + e^- \rightarrow Na$$

Chloride ion moves to the anode and chlorine is given off

$$2Cl^{-} + 2e^{-} \rightarrow CL_2$$

Reduction takes place at the negative chloride ie. There is electron gain while oxidation always takes place at the positive electrode ie there is electron loss.

In electrochemical cell, if the voltage across the cell is increased gradually and the current passing through the electrolyte measured. It was found that current remains very small until a certain voltage, it rises very quickly then the electrolysis start. The minimum voltage causing electrolysis to take place is called the decomposition voltage.

Electrodes placed into a solution will set up an electrode potential. The decomposition voltage s at least equal to the combination of the two electrodes potentials at the anode and cathode. Dnce, electrolysis is under way, there are significant changes in the concentration of the ions, near the electrode. This effect increases the decomposition voltage, so that it is larger than hat which might be calculated from electrode potential. The ions discharged during lectrolysis, you need to know their over voltage. (Phili Mathew, et'al)

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1 Fundamental Laws of Electrolysis

Product of electrolysis only appear on the surface of electrode and no where else in solution, because the electrolysis's the result of electron acceptance electron shedding nomena, and this can occur only at electrode surface.

The fundamental of electrolysis were investigated by MICHEAL FARADAY, the English sicist and chemist, discovered the two laws that bear his name, who laid down two ortant principles, which adapted to electrode position or electroplating, these are;

he amount of chemical substance (w) deposited at or dissolved from an electrode during trolysis is directly proportional to the quantity of electricity (Q) that passes through the ition.

i.e. $M \alpha Q$

But Q =It

the quantity of electricity (Q) is measured in column and current flown (I) measured in ere and time(t) in seconds.

Weight of deposition on electrode (W) =Z, I. t

Where z is the constant of proportionality and depends upon the characteristic of the species discharged at the electrodes. The constant is called the electrochemical valent of the ionic species and its unit is gram per coulomb.

ne electrochemical equivalent of an ionic species is its quality in grammes, which is ted from an electrode, passing one coulomb of electricity through the electrolyte.

hat when equal quantities of electricity (Q) pass through solutions of different electrolytes, amount of the substance (W) deposited or dissolved at the electrodes is directly prtional to the equivalent weight of the substance.(Assuming current efficiency of 100 ent).

he equivalent weight of a substance is its atomic weight divided by its oxidation number

Chemical equivalent = atomic weigh/valence.

By second law of faraday; when a current is passed through two electrolytes, if the deposits in two different electrolytes, electrode is W_1 and W_2 gm, and their equivalent weight is M_1 and M_2 , then.

 $W_1/W_2 = M_1/M_2$

2.2.2 Rate of Deposition

The minimum quantity of electricity required to deposit the equivalent weight in grammes of metal is 96500 will discharge 1 mole of hydrogen; this quantity of electricity is called faraday. One faraday is equal to one mole of electron since, the discharge of one mole of single charge ions involves the transfer of one mole of electron, which contains Avogadro's number i.e. 6.02 *10²³ of electrons.

Thus W = ItA/ZF

Where A is the atomic weight of metal deposited of valence, Z, F, is a constant called the faraday. The relation between atomic weight and chemical equivalent is; atomic weight = equivalent weight x valence.

The valence may be defined as being the number of atoms of hydrogen with which one atom of the element combines, or which it replaces. The figure is always a whole number, for example; silver is monovalent and cadmium divalent, or in other words, have valences of one and two respectively.

The faradays law of electrolysis can also be explained in terms of discharge of ion at the electrodes in electroplating, since electrons are involved in the discharge of an element.

2.3 Chemistry of Electroplating.

The quantity of products liberated at the electrodes during electroplating depends on three factors, which are the magnitude of the steady current, the time of flow of the steady current and the charge, of the liberated element. These quantitative aspects of electrolysis or electroplating were first investigated by faraday that later put forward two laws in 1833 to describe these quantitative relationships, these laws are called faraday laws of electrolysis.

Electroplating which involves electrolysis is guided by theories and laws. These are ionic heory, which was first presented by Arrhenius in 1887. Another law guiding electrolysis is the aradays law of electrolysis as earlier stated.

.3.1 The lonic Theory:

The ionic theory was first presented by Arrheniu in 1887 to explain electrolysis. The theory tated that when an electrolyte is molted or dissolved in water, some. If not all, of the nolecules of the substance dissociate (bread up) into freely morning charged particles called bns. The process of dissociation into ions is known as ionization e.g.

¢uSo₄

he metallic ions, like hydrogen and copper ion are positively charged. The number of lectrical charges carried by an ion is equal to the valence of the corresponding atom or roup. Due to electrical charges carried by these ions, their properties are quite different from nose of their corresponding atoms, which are electrically neutral. A metallic, for instances is prmed from the corresponding atom by the gain of a number of electrons equal to the alence of the atom.

When an electrolyte is dissolved in water or is melted, its molecules dissociate, or separate to freely moving ions. These free ions can exist independently of one another in solution, ut must of course always balance out electrically in other words, the numbers of positive and egatives charges must always be equal. Under the influence of a potential applied between vo electrodes immersed in the solution. (Cell voltage or cell potential) the ions will migrate, e positively charged ions towards the cathode or negative electrodes. The positive ions are ns are specifically known as cations i.e. cathode ions, at the cathode the cations gain ections and become uncharged atoms. Simultaneously, the negatives charged ions called hions, travel to anode. Where they give up electrons and also become uncharged atoms.

s a result of this transfer electron, uncharged atoms of the elements of which electrolyte is pmposed gather at the electrodes. Elements possessing positive oxidations number (metals) ccumulate at the cathode, element with negative oxidation number (non-metals) gather at e anode. In a deposition, although is continuously removed from the layer of electrolyte next to the cathode, the concentration of metal ions at the interfaces does not continuously decrease. A steady or equilibrium state is quickly reached because a number of natural agencies transport metal ions from the body of the bath to the cathode, to replace the ions deposited. These agencies are diffusion, convention and electrical migration. Electrical migration is the transport of ions under an applied electrical field (positive ion being attracted to the negative electrode and vice versa), contributes little to the transport of ions, as the speed of the ions is very small. The other two agencies, convection and diffusion transport most ions. These agencies do not rely upon an electrical field in order to operate. Convection is due to density gradients with the solution temperature.

Diffusions is the natural movement of ions from higher concentration to less concentrated regions of the electrolyte. Its effect is most pronounced in the regions of the electrolyte. Its effect is most pronounced in the regions of the electrolyte next of the cathodes (cathodes diffusions layer) from which the ions are continuously removed by deposition and replaced by ransport from bulk of the bath. Both diffusion and convention play a major role in the ransport of complex ions from body of bath to the cathode.

2.3.2. Electroforming

Electroforming is a variety of electro-deposition (deposition by electrolysis) in which an article o be reproduced is made conductive by spraying it with a metallic coaling, then electroplated with a metallic deposit in the normal way. The metallic deposits forms a mold, which is emoved from its base and filled into, reproduce the original article.

4.4. Preparation of the Object

he object to be plated must be thoroughly or surgically cleaned and rinsed before being placed in the plating bath. The surface must be of dirt; rust, oil and any oxides or other hemical impurities.

f such substances are not removed, the coaling may not adhere well to the surfaces. Grease and dirt are removed by organic solvent or alkaline solutions. Oxides are removed by organic olvent or alkaline solutions. Oxides are removed by organic solvent or alkaline solution.

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Oxides are removed by immersing the object in acid, the process is called pickling. In some cases the object is cleaned by making it the anode in an electrolytic process. This process is called electroplating.

2.5. Electrical Conductance of a Solution

Solution of sodium chloride, lime in water is good conduction of electricity, while solutions of sugar, area are bad conductor. To understand the difference in electrical conductance capacities for solutions, it is essential to know what was difference in conducting solutions as compared to a non-conducting one.

2.5.1 Presence of Ion and Electrical Conductance

Ordinarily metal wires are good conductors of electricity. This is due to easy availability of electrons in a metal and they have free electron. When an electric field is applied to a metal, according to the directions of applied field electrons starts moving from negative charged end of metal to its positive one, this is the way current flow in metal. In actual practice, it happens hat only electrons san move in a metal, larger practice, it happens that only electrons can move in a metal, larger particles (i.e. atomic nuclei or non metallic ions) cannot move through a metal. Thus, a substance conducts electricity when an electron or some other electrical charged particles like ion have to move through two types of electrically charged particles or ons. One type of ions negatively is called anions and other is positively charged and is called ations

3.5.2. Cathode and Anode

The metal plates dipped in a solution through which this electrons are liberated or absorbed, re called electrons. The electrons which liberates electrons from the solution after acquiring hem from negatively charged ions in the solution is positively charged and called the ANODE out the electrode which gives electrons to the solution (negatively charged is called CATHODE) of nickel plating. This double plating gives better production and the chromium idheres more strongly to the nickel than it does to most base metals. Zinc is the most eactive of all common metals it may however, be attached or dissolved by ordinary liquids such are soft drinks and vinegar. Therefore, materials that are plated with zinc are usually passivated with blue or yellow solution, that is finely covered with a solution that makes the surfaces passive to attack like oxidation, which can bring about tarnishing, in this project zinc (metal) was used for electroplating of basis metal.

2.6.1 General Application of Electroplating

For decorative plating metals used are Gold, Nickel, Chromium, Brass, Rhodium and Copper. For special decorative effect Tin, Zinc, Lead, Cadmium, Palladium and Platinum etc. are used. One metal may be plated over the basis metal or several metal may be plated one over the other on the basis metal. Metal, which forms basis metals, are steel, Brass, Copper, Nickel, Silver white metals alloys of lead or Tin base and Aluminum alloys.

2.6.2. Plating for Protection

Steel must be protected from rusting and chemical attack and so it is electroplated. Protective metals applied are Zinc, Cadmium and tin e.t.c. where both protection and good appearance. Nickel dulls by tarnish when exposed to atmosphere and chromium does not.

2.6.3. Plating for Special Surface and Engineering Effects

A part of a plant can be fabricated of an alloy, which is easy to fabricate and has got the required mechanical properties but is widely corroded when subjected to atmosphere of working. In such a case electroplating of the part with corrosion resisting metal serves their purpose very well.

Electroplating in engineering is employed for temporary use in metal treatment. For examples steel are parts before carbonizing are copper plated to prevent carbonization of undesired portions.

In hardening process, portion of steel are protected from nitrified by electroplating tin or copper-tin alloys on such portions

2.7 Electric Current

The electric current that is used in electroplating must be very carefully controlled in order to produce a smooth, eve, non-porous coaling of metal. The weight of metal deposited on the object and its average thickness deposited depends on the amount of electricity used and the time for which it flows.

2.7.1. Electrical Conductance of a Solution and Concentration of lons in it.

When an electric current is passed through a metallic conductor, according to the direction of the applied of the applied electrons flow as a stream in a single direction. This flow of current in an electrolyte (solution), have tow streams of cations and anions flowing in mutually opposite directions. But the total current strength is the sum of current strength due to the streams of cations and anions.

2.7.2 Electrolytes

This kind of electrolyte that is used for electroplating and its concentration has an important effect on the quality of coating. The electrolyte solution must be a good conductor of electricity and should not oxide when exposed to air. It should also have a good throwing power, the measure of its ability to coat all parts of the object close to the anodes. Even when the throwing power of the electrolyte is good the object is sometimes rotated during electroplating to make the coating more uniform. In many cases certain chemical, called brighteners, are added to the electrolyte to help make the coating brighter.

2.7.3 Metals Used in Electroplating

Nearly all metals can be used for electroplating. The most important are gold, silver, chromium, nickel tin, copper, cadmium lead and zinc (which this project really based on). Certain alloys, such as brass, nickel, cobalt and speculum, an alloy of tin and copper are also

used for plating. The most commonly used plating metal is nickel, because it is more resistant to corrosion than most of the other metals. Chromium plating, which is also very common, is usually applied on top of a layer.

2.8 Properties of Zinc

Zinc is a bluish-white lustrous metal, which is hard, crystalline and brittle. The metal is electronegative to ion and gives excellent corrosion resistances, particularly in industrial and urban environments. Zinc readily alloys with many other metals and one of the primary uses is in an alloy form for "zinc base die casting" which are of importance in the metal finishing trade. The "super plastic" alloys are also zinc based and can be blow-moulded.

Zinc is almost always deposited in the fully bought condition where an attractive and corrosions resistant finish is required; this can be subsequently passivated or dye, dissolving readily in dilute acids and alkalis therefore it is an unsuitable material for electroplating onto articles that are liable to come into contact with foodstuffs.

2.8.1 How a Layer of Zinc Prevent Iron Rusting

Of iron is dipped into molten zinc (at about 450°c) it gains a layer of zinc over its surfaces. Iron with its layer of zinc is said to be galvanized. There are two reasons why the zinc prevents iron rusting.

The first, most obvious, reason is that it prevents water and oxygen reaching the iron. The second, more interesting, reasons are that even if the zinc becomes partially worn away, it will still prevent rusting. Diagram below gives an idea of why this happens.

A some what similar situation rises to the zinc and copper in that case the copper was not worn; rather, it provided a path for this reaction of zinc with hydrogen ions to gives off hydrogen successfully. So it is with zinc and iron. Zinc has more electrode potential than iron (the values are $E_{zn}^{\theta}{}^{2+}/zn = -076v$, $E_{fe}^{\theta}{}^{2+}/fe = -0.44v$) therefore zinc will react according to the equation.

Zn (s)----->Zn²⁺ (aq) + 2e

Zinc is the anode. Zinc ions are converted into zinc hydroxide by hydroxide ions in the water. The elections directly between the zinc and the iron, which in this case is the cathodes. Where the iron is exposed to the surrounding water, hydrogen ions picks up the electrons.

•

2H⁺_(aq) + 2e → H₂ (9)

The point is that the iron remains unaffected; it is protect from the corrosion. A layer of zinc prevents iron from rusting. Instead of the Fe^{2r} ion going into solution, Zn^{z+} ions are lost from the zinc. The electrons release into the lattice joins with hydrogen ion in the water to make hydrogen. The hydrogen is produced at the iron surfaces. (J. J. Moore et'al)

3.0 METHODOLOGY

3.1. Equipment Used

- Electroplating bath
- Rectifier consisting of both voltmeter and Ammeter
- Beaker
- Oven (dryer)
- Digital weighing balance
- stop match

3.2. Materials Used

- Alkaline solution
- zinc cyanide
- Sodium cyanide
- HcL for pickling
- Distilled water
- Zinc anode
- Ferrous metal (cathode)
- Sodium chromate
- H2S04

Trioxonitrate acid

Brightener

3.2 Design of the Bath

The bath is made of thermoplastic cooler which will not react with the electrolyte and capable of containing 4 litres of electrolyte. The cathode wire is made of flat copper bored at interval, which was flitted on the thermoplastic cooler with the aid of glue and plastic insulating material. The plastic insulator aids in separating the cathode wire from the anode. The zinc



as connected to the positive copper wire while metal was connected to the negative copper ire.

3. Preparation of the Bath

he electrolyte is a mixture of 500g of sodium cyanide, 1kg of zinc cyanide, and 500g of odium hydroxide, 0.5 litre of zinc brightener and 2 litres of distilled water.

fter the solution (electrolyte) was made, it was left to stay for 24 hour so that the chemicals vill normalize.

he second step is the activation of carbon, which is for removing organic compound in the aths. The bath is allowed to stay for another 24hrs before it is free organic materials hence he bath is ready for use.

.4 Plating Procedure

lating procedure can be divided into three processing units

- 1. Pre-treatment
- 2. Electroplating
- 3. Post treatment

.4.1. Pre-Treatment (Cleaning of Base Metal)

ifferent materials had different pre-treatment procedure, which depends on the nature of the naterial. The nature of the base metal is very important for its pre-treatment. The nature of ontamination or the exposure is also important for efficient pre-treatment, pre-treatment or leaning of the base metal increase adhesion of the deposited metal. These are the following uppe of cleanliness.

- a. Physical cleanliness. If the surface of the metal is oily, greasy and rusty. It must be degreased at first. Grease greatly effects efficiency in mechanical chemical, therefore metals was freed from oil, grease and superficial dirt. This is done by using organic solvent such as tetrarchloride ethylene.
- b. Chemical cleanliness; the metal should be free from oxides or other compounds formed on the surface of the basis metal. This was achieved by dipping in acid solution

of 10-30% by volume, this is also known as "Acid Picking". The acid used is hydrochloric acid (HCL)

c. Mechanical cleanliness; the metal surface defeats such as scratches, and scans are removed by polishing. The metal should have no damaged surface, which is caused by mechanical operation. Sand paper was used so as to achieve better surface polishing the base metal improves adherence of electro-deposition.

3.5 Electroplating

,

After pre-treatment and water break on the basis metal, it was transferred to the racks into the electrolyte. The cathode is the ferrous metal, which is to be coated, zinc anode is the plating metal and the electrolyte is a zinc salt. Electroplating was carried out in a vessel, called the plating bath that contains the electrolyte.

The electrolyte is the zinc salt of the metal that is to form the coating. The base metal and zinc electrode are immersed in the electrolyte. The base metal is used as the cathode while the zinc metal is used as the anode. The base metal that is well cleaned was connected to the current source (rectifier) and is therefore "cathode". The zinc anode was connected **to** positive terminal and is therefore positive terminal and is therefore "zinc anode"

The positively charged metal ions, that is zinc ions from the zinc electrolyte are then moved and deposited on the basis metal (negative cathode) and are reduced to a metal atoms. The metal from the electrolyte is replaced by metal dissolved from the rod (zinc anode).

According to the theory of electrolysis; the amount deposited on the basis metal equals the amount dissolved from the zinc anode. After the required plating, the work piece was removed from the electrolyte and rinsed with distilled water and transferred to a well diluted trioxonitrate solution, which presents the plated metal from wearing out easily and finally the work piece was passivated and dry with a temperature rang of 40-50^oc in a dryer.

3.6 Composition of the Electrolyte

Zinc cyanide1kg
Sodium cyanide500g
Sodium hydroxide500g
0.5 litre of zinc brighter0.5 litres
Distilled water 2litres

3.7 Post Treatment

The plated metal is passed through a clean water to remove some of the ions attached to the work piece, and their pass through mild solution of trioxonitrate acid. Thus helps the plated surfaces from wearing out easily. It finally pass through a yellow passivation mixed a few drops of tetraoxosulpulphate (vi) acid. The metal is then ready for drying in a dryer with a temperature range of $40-60^{\circ}$ c for about 5 to 7 minutes.

Passivation concentration

Potassium chromate300g	
H ₂ 5045.0ML	
Distilled water1Litre	

¹ Soal clean



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4.0 RESULTS AND DISCUSSION

The results obtained are tabulated, the voltage, time of plating and current are recorded. Also current density and physical appearances were obtained. Different in weight of the metals with there corresponding thickness were also recorded. The temperature is at room temperature and the $P^{H of}$ electrolyte is 9.0.

4.1.0, Table Values of y at 1.1V and 1.0A with different time interval

S/NO	Voltage x ₁	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	observation
ine and the second s	1.1	5	1.0	5	0.53	11.5	11.60	0.100	7.32X10 ⁻⁴	Yellow
i wine and in the second strength of the second	1.1	7	1.0	7	0.53	11.4	11.54	0.140	9.50X10 ⁻⁴	Brownish yellow
	1.1	9	1.0	9	0.53	11.6	11.78	0.180	1.20X10 ⁻³	Bright yellow

S/NO	Voltage X1	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	observation
4	1.2	5 7	1.3 1.3	6.5 9.1	0.68 0.68	11.6 13.90	11.73 13.28	0.130 0.180	8.87x10 ⁻⁴	Yellow Brownish yellow
6	1.2	9	1.3	11.7	0.68	11.5	11.75	0.230	1.57x10 ⁻³	Bright yellow

4.1.2, Table Values of y at 1.4V and 1.5A with different time interval

S/NO	Voltage x ₁	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	l Initial Iwt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	observation
7 8	1.4	5	1.5 1.5	7.5 10.5	0.79 0.79	11.4	11.55	0.150 0.210	1.02x10 ⁻³	Yellow Brownish yellow
9	1.4	9	1.5	13.5	0.79	13.10	13.37	0.270	1.84x10 ⁻³	Bright yellow

4.1.3, Table Values of y at 1.8V and 2.0A with different time interval

S/NO	Voltage X1	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	observation
10	1.8	5.0	2.0	16.0	1.10	11.14	11.60	0.200	1.30x10 ⁻³	Bright
11	1.8	7.0	2.0	14.0	1.10	11.4	11.68	0.280	1.90x10 ⁻³	Bright
12	1.8	9.0	2.0	18.0	1.10	11.4	11.76	0.360	2.46x10 ⁻³	Bright

4.1.4, Table Values of y at 2.0V and 2.3A with different time interval

S/NO	Voltage ×1	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	observation
13	2.0	5.0	2.3	11.5	1.20	11.,5	11.73	0.230	1.57x10 ⁻³	Bright
14	2.0	7.0	2.3	16.1	1.20	11.6	11.92	0.320	2.18x10 ⁻³	Bright
15	2.0	9.0	2.3	20.7	1.20	11.5	11.92	0.420	2.46x10 ⁻³	Bright

4.1.5, Table Values of y at 2.2V and 2.5A with different time interval

S/NO	Voltage x ₁	Time(mins)	Current AMP	Coloumb It x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increase in wt (g)	Thickness Y (cm)	Observation
16	2.2	5	2.5	12.5	1.30	11.4	11.65	0.250	1.70x10 ⁻³	Bright
17	2.2	7	2.5	17.5	1.30	11.5	11.85	0.350	2.38x10 ⁻³	Bright
18	2.2	9	2.5	22.5	1.30	11.5	11.95	0.450	3.10x10 ⁻³	Bright

4.1.6, Table Values of y at 3.0V and 2.8A with different time interval

S/NO	Voltage x ₁	Time(mins)	Current AMP	Coloum b It= x ₂	ACM ⁻² Electric density	Initial wt (g)	Final wt (g)	Increas e in wt (g)	Thickness Y (cm)	Observati on
22	3.0	5.0	2.8	14.0	1.50	11.6	11.88	0.280	1.91x10 ⁻³	Yellow
23	3.0	7.0	2.8	19.6	1.50	11.5	11.90	0.400	2.73x10 ⁻³	Yellow
24	3.0	9.0	2.8	25.2	1.50	11.5	12.01	0.510	3.49x10 ⁻³	Yellow

4.1.7, Table Values of y at 3.5V and 3.0A with different time interval

S/NO	Voltage	Time(m	Curre	Coloumb	ACM ⁻²	Initial	Final wt	Increas	Thickness	Observati
	X 1	ins)	nt	It= x ₂	Electric	wt (g)	(g)	e in wt	Y (cm)	on
			AMP		density			(g)	 	
25	3.5	5.0	3.0	15	1.60	11.6	11.80	0.300	2.91x10 ⁻³	Yellow
26	3.5	7.0	3.0	21	1.60	11.6	12.02	0.420	2.73x10 ⁻³	Yellow
27	3.5	9.0	3.0	27	1.60	11.6	12.15	0.550	3.49x10 ⁻³	Yellow
4.2 Discussion of Results

In the experiment, the actual mass deposited or discharged at the cathodes are 0.100g, 0.140g, 0.108g, 0.130g, 0.180g, 0.230g, 0.150g, 0.210g, 0.270g, 0.200g, 0.280g, 0.360g, 0.230g, 0.320g, 0.420g, 0.250g, 0.350g, 0.450g, 0.270g, 0.380g, 0.490, 0.280, 0.400g, 0.510g, 0.300g, 0.420g, 0.550g, while the theoretical mass discharged are 0.1018g, 0.143g, 0.138g, 0.132g, 0.185g, 0.238g, 0.153g, 0.214g, 0.275g, 0.204, 0.285, 0.367g, 0.234 g, 0.328g, 0.422g 0.255g, 0.357 g, 0.458 g, 0.275g, 0.385g, 0.495g, 0.285g, 0.399g, 0.513g, 0.310g, 0.428 g, and 0.580g. These differences are the effect experimental such as inaccurate timing, improper agitation, etc. The mass of the deposited metal is directly proportional to the electricity supplied. The higher the quantity of the electricity the higher the deposited mass, for example, in table 4:1:0 the quantity of the electricity of 5, 7, and 9 coloumb has corresponding deposited mass of 0.100g, 0.140g and 0.180g respectively.

The thickness of the plated metal is also directly proportional to the deposited mass of the metal. The deposited masses of 0.100g, 0.140g, 0.108g, 0.130g, 0.180g, 0.230g, 0.150g, 0.210g, 0.270g, 0.200g, 0.280g, 0.360g, 0.230g, 0.320g, 0.420g, 0.250g, 0.350g, 0.450g, 0.270g, 0.380g, 0.490, 0.280, 0.400g, 0.510g, 0.300g, 0.420g, 0.550g, and its corresponding thickness of 7.32×10^{-4} cm, 9.50×10^{-4} cm, 1.20×10^{-3} cm, 8.87×10^{-4} cm, 1.20×10^{-3} cm, 1.57×10^{-3} cm, 1.43×10^{-3} cm, 1.84×10^{-3} cm, 1.30×10^{-3} cm, 1.90×10^{-3} cm, 2.46×10^{-3} cm, 1.57×10^{-3} cm, 2.18×10^{-3} cm, 2.46×10^{-3} cm, 1.70×10^{-3} cm, $2.38^{-1} \times 10^{-3}$ cm, 3.10×10^{-3} cm, 1.91×10^{-3} cm, 2.73×10^{-3} cm, 3.49×10^{-3} cm, 2.71×10^{-3} cm, 2.93×10^{-3} cm, and 3.49×10^{-3} cm.

From the experiment, it is observed that the thickness of the plated metal increases, the appearance of the finished material becomes less brighter.

4.3 Effect of Electric Density in the Experiment

In the experiment, rough surface of the base metal greatly reduced the expected current density. Activation and concentration polarization effect were observed to be directly dependent on the current density.

4.3.1 Effect of impurities in the experiment

Due to inaccurate information of pre-existing contamination such as inclusion in the base metal, cutting oils used and any organic or inorganic surface films, inadequate pre-treatment was given to the base metal which has effect on the metal finishing

4.3.2 Effect of improper agitation in the experiment

As a result of improper agitation of the electrolyte, there was excessive sludge built up, which affects the rate deposition to the base metal

4.3.3 Effect of voltage in the experiment

High voltage causes damage (burning) to the surface of the base metal; at voltage of 3.5volts, it was observed that coating of the base metal was not uniform, there was dark coloration at the surface of the metal. It was also observed as the voltage increases held constant, the thickness of the base metal decreases.

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Predicted Values of Y

S/NO	Voltag eX ₁	Time (mins.)(t)	Current(AM P)T	Coloub It=X ₂	Electr ic Densi ty	Change In wt(g)	Thickness Y ₁ (cm)	Observation
1	1.1	5	1.0	5	0.53	0.100	7.80x10 ⁻⁴	Yellow
2	1.1	7	1.0	7	0.53	0.140	9.60x10 ⁻⁴	Brownish yellow
3	1.1	9	1.0	9	0.53	0.180	1.14x10 ⁻³	Brownish yellow
4	1.2	5	1.3	6.5	0.68	0.130	9.50x10 ⁻⁴	Brownish yellow
5	1.2	7	1.3	9.7	0.65	0.180	1.20x10 ⁻³	Brownish yellow
6	1.2	9	1.3	11.7	0.68	0.230	1.40x10 ⁻³	Brownish yellow
7	1.4	5	1.5	7.5	0.79	0.150	1.10x10 ⁻³	Yellow
8	1.4	7	1.5	10.5	0.79	0.210	1.40x10 ⁻³	Yellow
9	1.4	9	1.5	13.5	0.79	0.270	1.7x10 ⁻³	Yellow
S/NO	Voltag eX ₁	Time (mins.)(t)	Current(AM P)T	Coloub lt=X ₂	Electr ic Densi	Change In wt(g)	Thickness Y ₁ (cm)	Observation

					ty			[
-								
10	1.8	5	2.0	10.0	0.75	0.200	1.50x10 ⁻³	Bright
11	1.8	7	2.0	14.0	1.10	0.280	1.80x10 ⁻³	Brighter
12	1.8	9	2.0	18.0	1.10	0.360	2.2x10 ⁻³	Brighter
13	2.0	5	2.5	11.5	1.10	0.250	1.70x10 ⁻³	Brighter
14	2.0	7	2.5	16.1	1.30	0.350	2.10x10 ⁻³	Brightest
15	2.0	9	2.5	. 20.7	1.30	0.450	2.51x10 ⁻³	Brighter
16	2.2	5	2.7	12.5	1.30	0.270	1.84x10 ⁻³	Bright
17	2.2	7	2.7	17.5	1.40	0.380	2.3x10 ⁻³	Bright
18	2.2	9	2.7	22.5	1.40	0.490	2.70x10 ⁻³	Bright
19	2.6	5	2.8	13.5	1.40	0.280	2.0x10 ⁻³	Bright
20	2.6	7	2.7	18.9	1.40	0.300	2.6x10 ⁻³	Bright
s/no	Voltag eX ₁	Time (mins.)(t)	Current(AM P)T	Coloum b It=X ₂	Electr ic Densi ty	Change In wt(g)	Thickness Y₁ (cm)	Observation
22	3.0	5	2.8	14.0	1.50	0.280	2.2x10 ⁻³	Yellow

23	3.0	7	2.8	19.6	1.50	0.400	2.8x10 ⁻³	Yellow
24	3.0	9	2.8	25.2	1.50	0.510	3.3x10 ⁻³	Yellow
25	3.5	5	3.0	15	1.60	0.300	2.50x10 ⁻³	Yellow
26	3.5	7	3.0	21	1.60	0.420	3.0x10 ⁻³	Yellow
27	3.5	9	3.0	27	1.60	0.550	3.6x10 ⁻³	Yellow

4.5 Discussion of Predicting Equation

Polymath 5:1 is a chemical engineering software use for general statistical analysis, using the software a response linear equation was derived for the experimental results. This is achieved by using general procedure with the aid of computer and making X_1 and X_2 impendent variables and Y_1 the dependent variables, which gives a linear regression equation show below:

 $Y_1 = -4.754E-05+3.452E-04X_1 + 9.01E-05X_2$

Substitution of X_1 and X_2 into the above linear equation will bring corresponding values of Y_1 as shown in the table below

Comparing the two process equation, there is a high degree of consistency with their orresponding values and the experimental values of Y. It was observed that their differences vere within acceptable limit with the variance is calculated to be 1.055 E-04. This means that ariance is close to zero. The correlation co-efficient is calculated to 0.95, which is very close 1, thus this simply means that the mathematics model best represents the experimental sta.

CHAPTER FIVE

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5.0 CONCLUSIONS AND RECOMMENDATION 5.1 CONCLUSION

The alm of this project is to zinc plate metals so as to increase harden ability and prevent them against corrosion, wear and tarnishing, which will serves as a decorative and protective functions. Metals were plated at various time and voltage and thickness was obtained.

Unlike most other commonly plated metals, zinc protects the substrate by sacrificing itself and thus corrodes before the base metal; this means that zinc will protect even if the zinc coating sustains minor damage; hence it was concluded that zinc coating with bright appearance which was yellow or blue passivated is good for engineering applications and of great importance in chemical process industries.

Electroplating process can be well understood with good knowledge of electrolysis as presented in this project with emphasis on the laws and theories that govern electrolysis.

5.2 RECOMMENDATION

Zinc is the most reactive of ail common metals, it, may however be attacked or dissolved by ordinary liquids such as soft drinks or vinegar. The ultimate corrosion resistance of zinc is a function of the plating thickness. To increase the corrosion resistance of zinc plating, a conversion coating is usually added, hence yellow or blue passivation. Therefore this project can be recommended for industries where corrosion resistance is needed so as to reduce the cost of preventing corrosion, also is good for decoration of the products in an industries, this will make it more attractive and generally accepted.

APPENDIX

1. Electric Density
$$\Rightarrow \frac{Current}{Geometric Area of the Electrode}$$

2. Current Efficiency

 $\Rightarrow \frac{\text{Actual mass deposited}}{\text{Theoritical mass discharge}} \times 100\%$

3. Theoretical mass Discharge $\Rightarrow M = \frac{\text{Wit}}{\text{nf}}$

Where w = molecular weight of element

I = current used

t = time of plating

n = valence of the atom

f = faraday.

. Thickness of the plated metal.

Weight = $mg \Rightarrow PVg \Rightarrow \int Ahg$

 $\Delta weight = \int_{fe} A.h.g$

$$h = \frac{\Delta weight}{\int_{fe} A_{fe} g}$$

Where h = thickness

 \int_{fe} = Density of iron

A_{fe} = Cross-sectional area of the base metal

g = Gravitational force

e multiple aggression equation for predicting Y values from X and x_2 values is

= a + b₁ x₁ + b₂ x₂

here a = $\overline{y} - b_1 \overline{x_1} - b_2 \overline{x_2}$

 $= y + b_1 (x_1 - \overline{x_1}) + b_2 (x_2 - \overline{x_2})$

=y + b₁ x₁+ b₂ x₂

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= Σ (x ₁)	y) (Σx²₂) -	-Σ(x ₂ y)	(Σx ₁ x ₂)					
(Σ	x ¹ ₂) (Σx ²	₂) – Σ(x·	$(x_2)^2$					
₂ = Σ (x2	!y) (Σx₁y)	(Σx ₁ x ₂)					•	
	12) (Σx ₂ ²)		_					
3		1						
ı = (126. 	.81x00-3)	(6914.	51) – (930x1	10-3) (876.76)				
r^{*}	((134.1)	(6914.51) –	(876.76)2				
1 = 3.45	2x10-4							
2 = (930	x10-3) (1	34.1) –	(126.81x10-	3) (87696)				
			(6914.51) –					
		(104.1)	(001101)	(0.0.0)=				
1 = 3.45								
₂ = (930)	x10 ⁻³) (13	94.1) — (126.81x10 ⁻³) (876.96)				
	. 1	(134.1)	(6914.51) –	(876.76) ²				
₂ = 9.01	8x10 ⁻⁵							
Vhere a	= y - b ₁ x	- b2 ¥	-					
				- 9.018x10 ⁻⁵ x1	4.96			
= 2.0	U14x10 ~	- 3.452	x10 °x2.09 ~	- 9.018X10 ° X1	4.00			
= - 4.75	54		•					
		X1		X2		Y	Mean	
				~4		1 '	INICALL	
aluable								
aluable 1	- <u></u>	134	.1	876.76		126.81x10 ⁻³	2.09	
		134	.1	876.76 6914.59	9	126.81x10 ⁻³ 930x10 ⁻³	2.09	
1		134	.1	•	9			
.1		134	1	•)	930x10 ⁻³	14.86	
1		134	.1	•)	930x10 ⁻³	14.86	
1 2 /				6914.59		930x10 ⁻³ 1237x10 ⁻⁴	14.86 2.014x10	
1 2 7 7/N X		4	X ₁ ²	6914.59	X ₁ x ₂	930x10 ⁻³ 1237x10 ⁻⁴ X y	14.86 2.014x10 X ₂ y	Y ²
1 2 / //N X 1	.1 5	5.0	X ₁ ² 1.21	6914.55 X ² 2 25.00	X ₁ x ₂ 5.50	930x10 ⁻³ 1237x10 ⁻⁴ X y 7.50x10 ⁻⁴	X ₂ y 3.41x10 ⁻³	Y ² 4.65x10 ⁻⁷
1 2 / //N X 1 1	.1 5 .1 7	4	X ₁ ²	6914.59	X ₁ x ₂	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻⁴ 1.05x10 ⁻³ 1.32x10 ⁻³	14.86 2.014x10 ⁻³ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶
1 2 7 7 1 1 1	.1 5 .1 7 .1 9	(1) (1) (1) (1) (1) (1) (1) 	X ₁ ² 1.21 1.21	6914.59 X ² 2 25.00 49.00 81.00 42.25	X ₁ x ₂ 5.50 7.70	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 7.50x10 ⁻⁴ 1.05x10 ⁻³ 1.32x10 ⁻³ 1.06x10 ⁻³	14.86 2.014x10 ⁻⁵ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷
1 2 7 1 1 1 1 1 1	.1 5 .1 7 .1 9 .2 6 .2 9	K ₁ 5.0 7.0 9.0 8.5 9.1	X ₁ ² 1.21 1.21 1.21 1.44 1.44	6914.55 X ² ₂ 25.00 49.00 81.00 42.25 82.81	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 7.50x10 ⁻⁴ 1.05x10 ⁻³ 1.32x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³	14.86 2.014x10 ⁻³ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶
1 2 7 1 1 1 1 1 1 1 1	.1 5 .1 7 .1 9 .2 6 .2 9 .2 1	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44	6914.59 X ² 2 25.00 49.00 81.00 42.25 82.81 136.89	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 7.50x10 ⁻⁴ 1.05x10 ⁻³ 1.32x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.88x10 ⁻³	14.86 2.014x10 ⁻³ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³ 18.37x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶
1 2 7 1 1 1 1 1 1 1 1 1 1	.1 5 .1 7 .1 7 .2 6 .2 9 .2 1 .4 7	K ₁ 5.0 7.0 9.0 5.5 9.1 1.7 7.5	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.44	6914.55 X ² ₂ 25.00 49.00 81.00 42.25 82.81 136.89 56.25	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 7.50x10 ⁻⁴ 1.05x10 ⁻³ 1.32x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.88x10 ⁻³ 1.48x10 ⁻³	14.86 2.014x10 ⁻³ 2.014x10 ⁻³ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³ 18.37x10 ⁻³ 7.65x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶
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1 2 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	.1 5 .1 7 .1 9 .2 6 .2 9 .2 1 .4 7 .4 7 .4 7	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.96 1.96 1.96	6914.55 X ² ₂ 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻³ 1.05x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 1.48x10 ⁻³ 2.00x10 ⁻³ 2.58x10 ⁻³	14.86 2.014x10 ⁻⁵ 2.014x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³ 18.37x10 ⁻³ 7.65x10 ⁻³ 15.02x10 ⁻³ 24.84x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶
1 2 7 7 8 7 8 7 7 7 7 7 7 7 7 7 7 7 7 7 7	.1 5 .1 .7 .1 .7 .2 .6 .2 .9 .2 .1 .4 .7 .4 .7 .4 .7 .8 .7	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.96 1.96 1.96 3.24	K ² 2 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25 100.00	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90 18.00	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻³ 1.05x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 1.48x10 ⁻³ 2.00x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 2.34x10 ⁻³	14.86 2.014x10 ⁻³ 2.014x10 ⁻³ 3.41x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³ 18.37x10 ⁻³ 7.65x10 ⁻³ 15.02x10 ⁻³ 13.00x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶ 1.69x10 ⁻⁶
1 2 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	.1 .5 .1 .7 .1 .9 .2 .6 .2 .9 .4 .7 .8 .7	K ₁ 5.0 7.0 9.0 5.5 9.1 1.7 7.5 10.5 13.5 10.0	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.44 1.96 1.96 1.96 1.96 3.24 3.24 3.24	6914.55 X ² ₂ 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.237x10 ⁻³ 1.05x10 ⁻³ 1.32x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 2.00x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 2.34x10 ⁻³ 3.42x10 ⁻³ 4.43x10 ⁻³	14.86 2.014x10 ⁻⁵ 2.014x10 ⁻³ 6.65x10 ⁻³ 10.8x10 ⁻³ 5.77x10 ⁻³ 10.92x10 ⁻³ 18.37x10 ⁻³ 7.65x10 ⁻³ 15.02x10 ⁻³ 13.00x10 ⁻³ 26.60x10 ⁻³ 44.28x10 ⁻³	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶ 3.61x10 ⁻⁶ 3.61x10 ⁻⁶ 6.05x10 ⁻⁶
1 2 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	.1 5 .1 .7 .1 .7 .2 .6 .2 .9 .4 .7 .8 .1 .8 .1 .0 .1	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.96 1.96 1.96 3.24 3.24 3.24 3.24 3.24	6914.55 X ² 2 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25 100.00 196.00 324.00 132.25	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90 18.00 25.00 32.40 23.00	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻³ 1.05x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 3.42x10 ⁻³ 3.42x10 ⁻³ 3.14x10 ⁻³	$\begin{array}{c c} 14.86\\ \hline 2.014 \times 10^{-5}\\ \hline 2.014 \times 10^{-5}\\ \hline 3.41 \times 10^{-3}\\ \hline 6.65 \times 10^{-3}\\ \hline 10.8 \times 10^{-3}\\ \hline 5.77 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 18.37 \times 10^{-3}\\ \hline 7.65 \times 10^{-3}\\ \hline 15.02 \times 10^{-3}\\ \hline 24.84 \times 10^{-3}\\ \hline 13.00 \times 10^{-3}\\ \hline 26.60 \times 10^{-3}\\ \hline 44.28 \times 10^{-3}\\ \hline 18.06 \times 10^{-3}\\ \hline \end{array}$	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶ 3.61x10 ⁻⁶ 3.61x10 ⁻⁶ 6.05x10 ⁻⁶ 2.43x10 ⁻⁶
1 2 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	.1 5 .1 .7 .1 .7 .2 .6 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .2 .9 .4 .7 .4 .7 .8 .1 .0 .1	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.44 1.96 1.96 1.96 3.24 3.24 3.24 3.24 4.00 4.00	6914.55 X ² 2 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25 100.00 196.00 324.00 132.25 259.21	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90 18.00 25.00 32.40 23.00 32.20	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻³ 1.05x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 2.00x10 ⁻³ 2.58x10 ⁻³ 2.34x10 ⁻³ 3.42x10 ⁻³ 3.14x10 ⁻³ 4.36x10 ⁻³	$\begin{array}{c c} 14.86\\ \hline 2.014 \times 10^{-5}\\ \hline 2.014 \times 10^{-5}\\ \hline 3.41 \times 10^{-3}\\ \hline 6.65 \times 10^{-3}\\ \hline 10.8 \times 10^{-3}\\ \hline 5.77 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 13.00 \times 10^{-3}\\ \hline 24.84 \times 10^{-3}\\ \hline 13.00 \times 10^{-3}\\ \hline 26.60 \times 10^{-3}\\ \hline 44.28 \times 10^{-3}\\ \hline 18.06 \times 10^{-3}\\ \hline 35.10 \times 10^{-3}\\ \hline \end{array}$	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶ 1.69x10 ⁻⁶ 3.61x10 ⁻⁶ 3.61x10 ⁻⁶ 2.43x10 ⁻⁶ 4.75x10 ⁻⁶
1 2 7 7 8 7 8 7 8 7 8 7 7 7 7 7 7 7 7 7 7	.1 5 .1 7 .1 7 .2 6 .2 6 .2 6 .2 6 .2 7 .4 7 .4 7 .4 7 .8 1 .8 1 .8 1 .0 1 .0 2	(1)	X ₁ ² 1.21 1.21 1.21 1.44 1.44 1.44 1.96 1.96 1.96 3.24 3.24 3.24 3.24 3.24	6914.55 X ² 2 25.00 49.00 81.00 42.25 82.81 136.89 56.25 110.25 182.25 100.00 196.00 324.00 132.25	X ₁ x ₂ 5.50 7.70 9.90 7.80 10.92 14.02 10.50 14.70 18.90 18.00 25.00 32.40 23.00	930x10 ⁻³ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1237x10 ⁻⁴ 1.05x10 ⁻³ 1.05x10 ⁻³ 1.06x10 ⁻³ 1.44x10 ⁻³ 1.44x10 ⁻³ 1.48x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 2.58x10 ⁻³ 3.42x10 ⁻³ 3.42x10 ⁻³ 3.14x10 ⁻³	$\begin{array}{c c} 14.86\\ \hline 2.014 \times 10^{-5}\\ \hline 2.014 \times 10^{-5}\\ \hline 3.41 \times 10^{-3}\\ \hline 6.65 \times 10^{-3}\\ \hline 10.8 \times 10^{-3}\\ \hline 5.77 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 10.92 \times 10^{-3}\\ \hline 18.37 \times 10^{-3}\\ \hline 7.65 \times 10^{-3}\\ \hline 15.02 \times 10^{-3}\\ \hline 24.84 \times 10^{-3}\\ \hline 13.00 \times 10^{-3}\\ \hline 26.60 \times 10^{-3}\\ \hline 44.28 \times 10^{-3}\\ \hline 18.06 \times 10^{-3}\\ \hline \end{array}$	Y ² 4.65x10 ⁻⁷ 9.03x10 ⁻⁷ 1.44x10 ⁻⁶ 7.87x10 ⁻⁷ 1.44x10 ⁻⁶ 2.47x10 ⁻⁶ 1.04x10 ⁻⁶ 2.05x10 ⁻⁶ 3.39x10 ⁻⁶ 3.61x10 ⁻⁶ 3.61x10 ⁻⁶ 6.05x10 ⁻⁶ 2.43x10 ⁻⁶

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18	2.2	22.5	4.84	506.25	49.50	6.82x10 ⁻³	69.75x10 ⁻³	9.61x10 ⁻⁶
19	2.6	13.5	6.74	182.25	35.00	4.78x10 ⁻³	24.84x10 ⁻³	3.39x10 ⁻⁶
20	2.6	18.5	6.74	357.27	49.14	6.73x10 ⁻³	48.95x10 ⁻³	6.71x10 ⁻⁶
21	2.6	24.3	6.74	590.49	63.18	8.68x10 ⁻³	81.16x10 ⁻³	1.12x10 ⁻⁶
22	3.0	14.0	9.00	196.00	42.00	5.73x10 ⁻³	26.74x10 ⁻³	3.65x10 ⁻⁶
23	3.0	19.6	9.00	384.16	58.80	8.19x10 ⁻³	53.51x10 ⁻³	7.45x10 ⁻⁶
24	3.0	25.2	9.00	635.04	75.60	10.47x10 ⁻³	87.95x10 ⁻³	12.18x10 ⁻⁶
25	3.5	15.0	12.25	225.00	52.50	7.18x10 ⁻³	30.75x10 ⁻³	4.20x10 ⁻⁶
26	3.5	21.0	12.25	441.00	73.50	10.01x10 ⁻³	60.05x10 ⁻³	8.18x10 ⁻⁶
27	3.5	27.0	12.25	729.00	93.50	13.13x10 ⁻³	10.25x10 ⁻³	14.06x10 ⁻⁶
Σ	56.4	401.1	134.10	6914.59	876.76	126.81x10 ⁻³	130.10 ⁻³	1.237x10 ⁻⁴

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REFERENCES

American Society of Quality Control (1990) "Metal Handbook" volume 2, Heat Treating, Cleaning and Finishing McGraw-Hill book company, New York, USA 6th Edition.

Ankerem E. N. (1993)" Introduction to Electroplating and Quality Control" Pg 1-3 Third edition.

- Encarta M. A. (1998) "Electroplating and Allied products" McGraw-Hill book company, New York, USA 2nd edition. Pg 17, 24-28.
- Graham (A. Kenneth Graham) (1978) "Electroplating Engineering Handbook" Third Edition, Van Nostrand Reeinhld (VNR) production London Pg 66-68, 190-191.
- J.J Moore Chemical Metallurgy Reed educational and professional publishing limited. Mel bourns Newelh Singapore. 2nd Edition Pg 221-224.

Leslie W. Flott "Quality Control in Electroplating" Pg 55 and 57.6th edition.

- M. M. Uppal A (1988) "Textbook for Engineering Chemistry". For engineering student KHANNA Publishers, India (pg. 558 and 564)
- Philip Matthews Advanced Chemistry Cambridge University press London low priced edition. Pg 408-410.
- Raymond Chang: Physical chemistry and its application, Macmillan publishing Co. Inc. New York second edition. Pp 214 278

Sedick Folashade Medinat (Dec. 2000) "Nickel Plating of Metals". Department of Chemical Engineering, FUT Minna.

 W. Kann & F. N. Spon "The Canning Handbook, Surface Finishing Technology Chemical Metals Electronic". 23rd edition. London Macmillan publishing co., Inc. New York. Pg 272 – 273, 293-320, 661-320 and 70⁷-708.

GLOSSARY OF ELECTROPLATING

Activation: Elimination of a passive condition on a surface.

Adhesion: (1) the attractive force that exists between an electrodeposits and its substrate.

(2) The force required separating electrodeposits from its substrate.

Alloy: A substance having metallic properties composed of two or more elements of which at least one is a metal

Anion: Anion, which is negatively charged.

Anode: The electrode at which current enters or electrons leaves the solution; the positive electrode in electrolysis, the electrode at which negative ions are discharged, positive ions are formed, or at which other oxidizing reactions occur.

Anodizing: Anodic treatment of metals, particularly aluminium to form an oxide film of controlled properties.

Brightener: An addition agent, winch leads to the formation of a bright plate; or which improves the brightness of the deposit over that which is obtained without its use.

Cathode: The electrode through which current leaves, or electrode in electrolysis. The electrodes at which positive ions are discharged, negative ions are formed, or other reducing reactions occur. In electroplating, the electrode which receives the deposit.

Chemical pickling: The surface layer is removed from metal by chemical pickling.

Cleaning: The removal of grease in which a current is passed through the solution, the work being one other electrode.

Solvent; Cleaning by means of organic solvents.

Coating: A protective layers.

Corrosion: (I) Gradual destruction of a material usually by solution. Oxidation or other means attributable to a chemical process.

2)(Of anodes in plating) solution of anode metal by the electrochemical action in the plating cell.

Degreasing: The removal of grease and oils from a surface by using solvent.

Brag-In: The water of solution that adheres to the objects introduced into a bath. Brag-out: The solution that adheres to the objects removed from a bath.

lectrode: A conductor of the metallic class through which a current enters or leaves arm

electrolytic cell; at which there is a change from conduction by electrons to conduction by

particles of matter, or vice versa